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Megan C. Shade

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## **THE EFFECT OF MOLAR PEROXIDE RATIO ON THE OXIDATION OF BISPHENOL A IN AN ULTRAVIOLET LIGHT EMITTING DIODE/HYDROGEN PEROXIDE ADVANCED OXIDATION PROCESS**

THESIS

Megan C. Shade

**DEPARTMENT OF THE AIR FORCE AIR UNIVERSITY**

# *AIR FORCE INSTITUTE OF TECHNOLOGY*

**Wright-Patterson Air Force Base, Ohio**

APPROVED FOR PUBLIC RELEASE; DISTRIBUTION UNLIMITED

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## **THE EFFECT OF MOLAR PEROXIDE RATIO ON THE OXIDATION OF BISPHENOL A IN AN ULTRAVIOLET LIGHT EMITTING DIODE/HYDROGEN PEROXIDE ADVANCED OXIDATION PROCESS**

## THESIS

Presented to the Faculty

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In Partial Fulfillment of the Requirements for the

Degree of Master of Science in Environmental Engineering and Science

Megan C. Shade, BS

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### APPROVED FOR PUBLIC RELEASE; DISTRIBUTION UNLIMITED

#### AFIT-ENV-MS-21-M-271

## THE EFFECT OF MOLAR PEROXIDE RATIO ON THE OXIDATION OF BISPHENOL A IN AN ULTRAVIOLET LIGHT EMITTING DIODE/HYDROGEN PEROXIDE ADVANCED OXIDATION PROCESS

Megan C. Shade

### NH-02

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Dr. Willie F. Harper, Jr. Chair

Dr. Adam C. Burdsall Member

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#### **Abstract**

Bisphenol A (BPA) is a compound widely used in industry that is detrimental to human health and ecological systems. It enters the environment through various process and subsequently creates an exposure hazard. Ultraviolet light emitting diodes (UVLED) and hydrogen peroxide  $(H_2O_2)$  can be combined to create an advanced oxidation process that produces hydroxyl radicals. These highly reactive radicals have the potential to degrade contaminants in water. Further knowledge of the optimal molar peroxide ratio to effectively degrade contaminants and any subsequent reaction byproducts is needed. This research utilized 50, 100, 250, 500, and 1000:1 H2O2:BPA molar ratios in a Continuous Flow Stirred-Tank Reactor (CFSTR) with UVLED as the mechanism for BPA degradation. High Performance Liquid Chromatography (HPLC) and Mass Spectrometry (MS) were used for the analysis of mass ratio concentrations and potential reaction byproducts, respectively. This study saw the highest degradation and rate constants at the 500:1 molar ratio. The 100 and 250:1 ratios had similar rate constants and degradation, both slightly lower than the 500:1 ratio. The 50 and 1000:1 ratios were also similar to each other and had the lowest degradation and rate constants. These results illustrate that the reactions at the 50, 100, and 250:1 ratios were hydrogen peroxide limited. The 1000:1 results exhibited evidence of radical scavenging that limited the degradation of BPA. Further research at molar peroxide ratios near the 100, 250, and the 500:1 ratio could provide the best potential for BPA removal versus cost or regulatory requirements.

To my family, your unwavering support, wisdom, and love brought me to this point. Your compassion, and concern for others inspired me to make a difference in the world. To my friends who believed in me and cheered me on. And to my pitbulls, my study partners that never left my side. It has been an honor to have you in my life.

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## **Table of Contents**



## **List of Figures**



## **List of Equations**

Equation 1: Reaction Rate Constant Equation 22

## **List of Tables**

Table 1: Reaction rate constants 40

**Page**

## **Glossary of Acronyms and Abbreviations**

- AFIT Air Force Institute of Technology
- AOP Advanced Oxidation Process

BPA – Bisphenol A

CEC – Contaminants of Emerging Concern

CFSTR – Continuous Flow Stirred-Tank Reactor

- DI Water Deionized water
- HO∙ Hydroxyl Radical
- HPLC High Performance Liquid Chromatography
- H2O2 Hydrogen Peroxide
- LED Light Emitting Diode
- MS Mass Spectroscopy
- UV Ultraviolet
- WPAFB Wright Patterson Air Force Base
- WWTP Wastewater Treatment Plant

### **THE EFFECT OF MOLAR PEROXIDE RATIO ON THE OXIDATION OF BISPHENOL A IN AN ULTRAVIOLET LIGHT EMITTING DIODE/HYDROGEN PEROXIDE ADVANCED OXIDATION PROCESS**

#### **I. Introduction**

#### **1.1 Chapter Overview**

This chapter summarizes the need for this research, defines the problem, the hypothesis, and how this experiment was conducted.

#### **1.2 General Issue**

Global water resources have been inundated with various pollutants. Pathogens, pesticides, pharmaceuticals, solvents, chlorinated organics, and algal toxins are some of the many hazardous substances that are harmful to both human health and the environment. Current wastewater treatment plants (WWTP) provide minimal removal of these compounds. When the wastewater effluent is discharged, it introduces these pollutants into waterways (Kang et al., 2018). This presents a need for further research into treatment technologies that can remediate various pollutants without creating toxic byproducts. Contaminants of concern (CEC) in water sources have increased due to rises in chemical production and human populations. Additionally, improvements in analytical technology have highlighted chemical levels that were previously undetected, further expanding the number of compounds now found throughout the environment (Baken et al., 2018). These CEC originate from pharmaceutical and personal care products, pesticides, industrial compounds, and illicit drugs, and have known/potential adverse health and environmental effects (Borull et al., 2019).

BPA is widely used in various industry processes and products that has resulted in pervasive exposure to both humans and the environment. It is a known endocrine disruptor that has also exhibited additional potential adverse effects to human health and ecological systems (Wang et al., 2009). Wastewater treatment generally has low BPA removal rates leading to the release of the compound during discharge (Kang et al., 2018). This has led to an intensified need for treatment and remediation technologies.

Safe drinking water is essential for the military, not only in the United States, but abroad as well. Environmental security has been a priority for the military since the 1990s, and water issues are considered a threat to national security (O'Lear et al., 2013). Further understanding of technology with the potential to protect, as well as treat water resources is essential to human health and military capabilities.

Ultraviolet (UV) Light Emitting Diodes (LED) and Hydrogen peroxide  $(H_2O_2)$ have the potential to be utilized in the application of an Advanced Oxidation Process (AOP) during the water treatment process. When  $H_2O_2$  is exposed to UV light it creates two hydroxyl radicals (HO∙) that are highly reactive (Vega & Valdés, 2018). This research studied the results of BPA degradation when treated with various molar ratios of H2O2 to BPA.

Mercury lamps have been utilized in water treatment, but they pose additional environmental concerns. LED technology presents an alternative to the traditional mercury lamps.

#### **1.3 Problem Statement**

The Air Force Institute of Technology (AFIT) at Wright-Patterson Air Force Base (WPAFB) is researching the degradation potential of contaminants during  $H_2O_2$  UV LED AOP. BPA is a contaminant that has been routinely observed in source/drinking water, and can enter the environment through wastewater discharge and sludge (Kleywegt et al., 2011). The effects of UV LED-AOPs on BPA removal are not fully understood and require additional research.

#### **1.4 Research Objectives**

The purpose of this research was to study the effect of molar peroxide ratio on BPA removal during an AOP and investigate the production of reaction byproducts. BPA removal kinetics are expected to be influenced by hydroxyl radical scavenging. Radical scavenging can interfere with the radical-BPA reactions, thereby inhibiting the degradation mechanisms.

#### **1.5 Methodology**

During the course of this research, one control experiment, and 15 AOP experiments were conducted. The control test was completed without the addition of H2O2. The 15 AOP experiments consisted of five molar ratios (50, 100, 250, 500, and 1000:1 H2O2 to BPA). These AOP experiments consisted of two 60-minute segments. The first hour was completed without UV light, and the solution was recycled back to the original flask. Samples were taken at time 0, 10, 20, 30, 40, 50, and 60 minutes. After the initial 60 minutes, the UV light was turned on and samples were collected at time 0, 2, 4,

6, 10, 15, 20, 25, 35, 45, and 60 minutes. The solution was pumped into a waste container after passing through the reactor. Each molar peroxide ratio was replicated for three trials. Each sample was collected and filtered into High Performance Liquid Chromatography (HPLC) vials. The samples were analyzed using HPLC and Mass Spectroscopy (MS). The HPLC data was used to determine BPA concentrations and the MS data was used to determine possible by-products. Tukey pairwise comparisons were used for statistical analysis utilizing Jupyter Notebook 6.0.1.

### **1.6 Assumptions and Limitations**

There were several assumptions made for this research:

- 1. The components of the experiment were working at the same efficiency for each trial.
- 2. The stir bar maintained a consistently mixed solution inside the reactor. Observations were made to determine if it was likely the stir bar was continuing to operate; checking the reactor for vibrations and listening for noise associated with the stir bar spinning inside the reactor.

#### **II. Literature Review**

#### **2.1 Chapter Overview**

This chapter summarizes BPA fate in the environment, potential problems of BPA, and the AOP process.

#### **2.2 Background**

Bisphenol A is a known endocrine disruptor that may have additional adverse effects to human health and ecological systems (Wang et al., 2009). It has been utilized in the production of wide-ranging items, and during industrial processes, including the food and beverage industry (Hu et al., 2019). Because BPA is widely used, is present in various environmental media, and has detrimental effects, it is necessary to further research remediation and treatment options. BPA has a molecular weight of 228.29 g/mol and molecular formula  $C_1<sub>5</sub>H<sub>16</sub>O<sub>2</sub>$ . The molecular structure of BPA (Figure 1) has two benzene rings each containing a hydroxyl group, which form a phenol, connected by a central carbon atom. Two methyl groups are also located at the central carbon atom.

**Figure 1: BPA molecular structure**



Due to the pervasive use of BPA in industry, this chemical is released into the environment via various mechanisms. The processes that produce BPA, and the subsequent wastewater discharges are categorized as production sources. Landfill leaching, degradation of plastics already in the environment, WWTP discharges, and disposal or burning of waste are considered consumer sources (Corrales et al., 2015). BPA has been detected in the influent and effluent of wastewater treatment plants, as well as in sewage sludge. Sewage sludge utilized as fertilizer can introduce BPA into the food supply and groundwater (Hu et al., 2019). BPA has also been observed in source water and drinking water (Kleywegt et al., 2011)

Mercury lamps have routinely been used to generate UV light for water treatment processes and previous AOP research, but UV LED options are increasingly seen as a better option. UV LED lamps are highly energy efficient compared to the standard mercury lamps (Martín-Sómer et al., 2017). Mercury is a known toxin and is highly detrimental to human health (Bjørklund et al., 2017). Mercury lamps are also very fragile and have higher operating costs than LEDs (Huang et al., 2017).

#### **2.3 BPA Degradation Research**

Previous studies of BPA degradation have utilized both hydroxyl and sulfate radicals during AOP research, with both radicals showing sufficient ability to remove BPA from water (Qui et al., 2019). These studies have varied in their approach, as well as the parameters the researchers were analyzing. Carbonate and nitrate constituents are found in natural waters; BPA degradation levels and reaction byproducts varied when combined with these constituents (Kang et al., 2018). Titanium dioxide (TiO<sub>2</sub>), when

used as the photocatalyst, has also shown to degrade BPA in an AOP. The removal rates decreased as the amounts of TiO<sub>2</sub> oversaturated the solution (Wang et al., 2009). BPA degradation has also been demonstrated with UV light only, increasing as the drive current increases (Stubbs, 2017).

BPA removal has also been conducted utilizing adsorption technologies. Different adsorptive media, such as clays, activated carbon, natural polymers, and nanomaterials have had success in removing BPA from water sources (Bhatnagar and Anastopoulos, 2017).

The limited research completed thus far showcases the need for additional data collection under this study's parameters.

#### **III. Methodology**

#### **3.1 Chapter Overview**

This chapter details the materials and methods used to conduct the AOP experiments.

#### **3.2 Materials and Equipment**

250 mL Pyrex $\&$  Vista<sup>TM</sup> No. 70640 volumetric flasks were used for solution preparation and storage. PharMed® BPT tubing circulated the solution from the flasks to the Continuous Stirred-Tank Reactor (CSTR), and from the CSTR to the flask. To maintain constant mixing, a stir bar and stir plate were utilized with both the solution flask and the reactor. A Cole-Parmer® MasterFlex® No. 77200-50 peristaltic pump propelled the solution through at a rate of 2 mL per minute. The pump was primed with a 45 mL of solution using a 60 mL syringe. Electricity was provided to the reactor by Keysight E3620A Dual Output DC Power Supply. A Mettler-Toledo pH meter was used to determine the pH of the  $H_2O_2$  - BPA solution before it was circulated through the reactor. Each sample was captured in a syringe and filtered with a Millex® - FG Hydrophobic Fluoropore™ 0.2 µm filter into HPLC vials. All samples and standards were vortex mixed for 30 seconds on a Daigger Vortex Genie 2® mixer. HPLC and MS were conducted on an Agilent technologies 6130 Quadrupole LC/MS.

#### **3.3 Hydrogen Peroxide/BPA Molar Ratio Experiment**

Five molar ratios, 50, 100, 250, 500, and 1000:1  $H_2O_2$  to BPA were utilized to study the effects molar peroxide ration on BPA degradation. 31 mL of 81 mg/L BPA

solution was pipetted into a 250 mL flask and filled with Deionized (DI) water to create a 10 mg/L BPA solution. 30% hydrogen peroxide stock solution was added to the flask at volumes of 55, 11, 277, 111, 554, 1108 µL to produce the 50, 100, 250, 500, and 1000:1 molar ratios respectively. A stir bar was added to the solution before the flask was wrapped in foil, hand mixed for 10 minutes, and then placed on a stir plate at 850 rpm for one hour. 100, 200, 400, 600, 800, and 1000  $\mu$ L of the H<sub>2</sub>O<sub>2</sub> – BPA solution were pipetted into HPLC vials to create standards of 10, 20, 40, 60, 80, and 100% respectively. A blank was created using DI water. All standards were filtered and vortex mixed for 30 seconds.

To prepare the reactor setup, the tubing was connected to the entry and exit ports of the reactor and primed with 45 mL of solution. The stir plate for the reactor was turned on. The UVLED electrical source was preadjusted to 0.068 amps. The flask containing the  $H_2O_2$  – BPA solution was placed on a stir plate adjacent to the reactor and maintained at 850 rpm.

To obtain the control samples, the pump was turned on at time zero minutes and the first sample was collected. Control samples were collected at time 0, 10, 20, 30, 40, 50, and 60 minutes. Each sample was filtered into a HPLC vial and vortex mixed for 30 seconds. During the control portion of the experiment, the effluent was recycled back into the solution flask.

After the control samples were collected, the UV light was turned on and the first sample was collected at time 0 minutes. Experiment samples were taken at time 0, 2, 4, 6, 10, 15, 20, 25, 35, 45, and 60 minutes. Each sample was filtered into a HPLC vial and

vortex mixed. During the run portion of the experiment, the effluent was cycled into a waste container. Once the standards and samples were obtained, they were placed into the HPLC tray. The HPLC program was loaded and verified before starting the analysis.

Reaction rates were acquired using a reaction rate derivation in MATLAB code created by Dr. Harper.

## **Equation 1: Equation for reaction rate constants**

$$
C_n/C_0 = \frac{(1 + \tau k) * e^{(1/\tau + k)*(-1)t}}{\tau k + 1}
$$



**Figure 2: Continuous Flow Stirred-Tank Reactor**



**Figure 3: AOP Experiment setup – effluent recycled into solution flask**

The recycled reactor set up was utilized during the control portion of each AOP.



**Figure 4: AOP Experiment setup – effluent cycled into waste container**

The non-recycled reactor setup was utilized for the initial control without H<sub>2</sub>O<sub>2</sub>, and all

AOP runs during UV exposure.

#### **IV. Analysis and Results**

#### **4.1 Chapter Overview**

This chapter discusses the results and statistical analysis of the AOP experiments.

#### **4.2 Results**

Figure 5 shows the mass ratios of a BPA solution without any added  $H_2O_2$ , a 0:1 ratio. The x-axis is the time elapsed for the duration of the experiment. The y-axis is the relative concentration  $(C_n/C_0)$  of BPA. For the control, four samples were taken with no UV light. The control was conducted to illustrate if the treatment had an effect on BPA degradation. The UV light was turned on and eight samples were taken for the trial.

The relative concentrations of the control at time 0, 20, 40, and 60 minutes were 0.84, 0.88, 0.85, 0.86 respectively. The relative concentrations remain overall consistent during the 60-minute control time. The results of the relative concentrations of the control illustrate the experiment did not degrade BPA.

The relative concentrations of the trial at time 5, 10, 15, 20, 25, 35, 45, and 60 minutes were 1.04, 1.04, 1.00, 1.00, 1.00, 0.99, 1.01, and 1.02 respectively. The results of the relative concentrations of the trial illustrate the experiment did not degrade BPA when exposed to UV light without  $H_2O_2$  added to the solution.





Figure 6 shows the degradation of BPA in three trials at the  $50:1 \text{ H}_2\text{O}_2$  to BPA molar ratio. The x-axis is the time elapsed for the duration of the experiment. The y-axis is relative concentration  $(C_n/C_0)$  of BPA. For the control, seven samples were taken with no UV light. The UV light was turned on and eleven samples were taken for the trial.

The average relative concentrations of the controls at time 0, 10, 20, 30, 40, 50, and 60 minutes were 0.90, 0.90, 0.89, 0.91, 0.90, 0.89, and 0.91, respectively. The control did not degrade BPA with the UV light off. The average relative concentrations of the trials at time 0, 2, 4, 6, 10, 15, 20, 25, 35, 45, and 60 minutes were 0.98, 0.73, 0.65, 0.55, 0.42, 0.38, 0.33, 0.34, 0.31, 0.30, 0.29 respectively.

The majority of degradation occurred during the first ten minutes, leveling out throughout the remainder of the experiment as the solution in the reactor reached equilibrium. The results of the relative concentrations of the trial illustrate the experiment degraded BPA. The lack of degradation during the control compared to the degradation exhibited during the trials shows that the  $H_2O_2$ -UV treatment was effective.



## **Figure 6: Hydrogen Peroxide:Bisphenol A 50:1 Mass Ratio vs Time**

Figure 7 shows the degradation of BPA in three trials at the  $100:1 \text{ H}_2\text{O}_2$  to BPA molar ratio. The x-axis is the time elapsed for the duration of the experiment. The y-axis is the relative concentration  $(C_n/C_0)$  of BPA. For the control, seven samples were taken with no UV light. The UV light was turned on and eleven samples were taken for the trial.

The average relative concentrations of the controls at time 0, 10, 20, 30, 40, 50, and 60 minutes were 0.91, 0.93, 0.92, 0.93, 0.93, 0.94, and 0.94, respectively. The control did not degrade BPA with the UV light off. The average relative concentrations of the trials at time 0, 2, 4, 6, 10, 15, 20, 25, 35, 45, and 60 minutes were 0.98, 0.69, 0.50, 0.39, 0.29, 0.25, 0.25, 0.22, 0.25, 0.24, 0.21 respectively.

The majority of degradation occurs during the first ten minutes, leveling out throughout the remainder of the experiment as the solution in the reactor reached equilibrium. The results of the relative concentrations of the trial illustrate the experiment degraded BPA. The lack of degradation during the control compared to the degradation exhibited during the trials shows that the  $H_2O_2$ -UV treatment was effective.

 The 26 June trial experienced pump issues at the 25- and 35-minute sample times. The 25 min sample was collected at 27 minutes and the 35 min sample was collected at 36 minutes.



## . **Figure 7: Hydrogen Peroxide:Bisphenol A 100:1 Mass Ratio vs Time**

Figure 8 shows the degradation of BPA in three trials at the  $250:1$  H<sub>2</sub>O<sub>2</sub> to BPA molar ratio. The x-axis is the time elapsed for the duration of the experiment. The y-axis is the relative concentration  $(C_n/C_0)$  of BPA. For the control, seven samples were taken with no UV light. The UV light was turned on and eleven samples were taken for the trial.

The average relative concentrations of the controls at time 0, 10, 20, 30, 40, 50, and 60 minutes were 0.89, 0.90, 0.91, 0.90, 0.90, 0.89, and 0.91, respectively. The control did not degrade BPA with the UV light off. The average relative concentrations of the trials at time 0, 2, 4, 6, 10, 15, 20, 25, 35, 45, and 60 minutes were 0.97, 0.57, 0.49, 0.39, 0.30, 0.24, 0.24, 0.24, 0.24, 0.25, 0.24 respectively. This molar ratio had degradation comparable to the 100:1 ratio.

The majority of degradation occurs during the first ten minutes, leveling out throughout the remainder of the experiment as the solution in the reactor reached equilibrium. The results of the relative concentrations of the trial illustrate the experiment degraded BPA. The lack of degradation during the control compared to the degradation exhibited during the trials shows that the  $H_2O_2$ -UV treatment was effective.



## **Figure 8: Hydrogen Peroxide:Bisphenol A 250:1 Mass Ratio vs Time**

Figure 9 shows the degradation of BPA in three trials at the 500:1  $H_2O_2$  to BPA molar ratio. The x-axis is the time elapsed for the duration of the experiment. The y-axis is the relative concentration  $(Cn/C0)$  of BPA. For the control, seven samples were taken with no UV light. The UV light was turned on and eleven samples were taken for the trial.

The average relative concentrations of the controls at time 0, 10, 20, 30, 40, 50, and 60 minutes were 0.85, 0.86, 0.89, 0.88, 0.90, 0.87, and 0.86, respectively. The control did not degrade BPA with the UV light off. The average relative concentrations of the trials at time 0, 2, 4, 6, 10, 15, 20, 25, 35, 45, and 60 minutes were 0.96, 0.60, 0.42, 0.29, 0.22, 0.19, 0.19, 0.13, 0.13, 0.19, 0.18 respectively. This molar ratio had the highest degradation compared to the other ratios.

The majority of degradation occurs during the first ten minutes, leveling out throughout the remainder of the experiment as the solution in the reactor reached equilibrium. The results of the relative concentrations of the trial illustrate the experiment degraded BPA. The lack of degradation during the control compared to the degradation exhibited during the trials shows that the  $H_2O_2$ -UV treatment was effective.

The 500:1 results indicate that the 100:1 and 250:1 results were limited due to the levels of hydrogen peroxide. The addition of more hydrogen peroxide facilitates more radical production, resulting in greater BPA degradation.

 The 10 July trial experienced pump issues at the 25- and 35-minute sample times. The 25 min sample was collected at 26 minutes and the 35 min sample was collected at 36 minutes



## **Figure 9: Hydrogen Peroxide:Bisphenol A 500:1 Mass Ratio vs Time**
Figure 10 shows the degradation of BPA in three trials at the  $1000:1 \text{ H}_2\text{O}_2$  to BPA molar ratio. The x-axis is the time elapsed for the duration of the experiment. The y-axis is the relative concentration  $(C_n/C_0)$  of BPA. For the control, seven samples were taken with no UV light. The UV light was turned on and eleven samples were taken for the trial.

The average relative concentrations of the controls at time 0, 10, 20, 30, 40, 50, and 60 minutes were 0.89, 0.91, 0.90, 0.90, 0.90, 0.92, and 0.91, respectively. The control did not degrade BPA with the UV light off. The average relative concentrations of the trials at time 0, 2, 4, 6, 10, 15, 20, 25, 35, 45, and 60 minutes were 0.98, 0.69, 0.56, 0.48, 0.34, 0.32, 0.29, 0.28, 0.31, 0.30, 0.30 respectively. This molar ratio had degradation comparable to the 50:1 ratio, both having the lowest BPA removal.

The majority of degradation occurs during the first ten minutes, leveling out throughout the remainder of the experiment as the solution in the reactor reached equilibrium. The results of the relative concentrations of the trial illustrate the experiment degraded BPA. The lack of degradation during the control compared to the degradation exhibited during the trials shows that the  $H_2O_2$ -UV treatment was effective.

These results strongly suggest that radical scavenging occurred. Because the solution was comprised of DI water,  $H_2O_2$ , and BPA, there are three possible radical scavengers: bicarbonate,  $H_2O_2$ , and other radicals. Radical-radical reactions are the most thermodynamically favorable with an activation energy of 8 kJ/mol. Radical-H<sub>2</sub>O<sub>2</sub> reactions have the next lowest activation energy at 14 kJ/mol followed by radicalbicarbonate at 23.6 kJ/mol (Buxton et al., 1988)

36



**Figure 10: Hydrogen Peroxide:Bisphenol A 1000:1 Mass Ratio vs Time**

Figure 11 shows the averages of the five molar ratios in comparison to each other. The x-axis represents the time elapsed for the duration of the experiment. The y-axis represents the relative concentration. The 500:1 ratio had the highest degradation followed by 100 and 250 ratios. The 50 and 1000 ratios had the lowest degradation of all the ratios. The error bars have a value of one standard deviation.

A previous AOP study conducted at AFIT by Col John E. Stubbs, utilized the same reactor setup as this research, and demonstrated that BPA removal is a function of molar peroxide ratio (Stubbs, 2017).



**Figure 11: Comparison of averages of the five molar ratios**

Table 1 shows the rate constants generated for each experiment and the average for each ratio. The 500:1 molar ratio had the highest average rate constant. The 100 and 250 molar ratios averages were very close to each other and were the second highest rate. The 50 and 1000 ratios were also similar to each other and were the lowest rates out of the five molar ratios.

	1000:1	500:1	250:1	100:1	50:1
	0.17	0.31	0.3	0.17	0.16
	0.15	0.26	0.2	0.19	0.12
	0.14	0.26	0.15	0.26	0.11
<b>AVG</b>	0.15	0.28	0.22	0.21	0.13

**Table 1: Reaction rate constants**

Tukey pairwise comparison statistical analysis was utilized to determine statistical differences between overall degradation of the molar ratios and the rate constants of the molar ratios. The significance level for the analysis was 0.05 which corresponds to a 95% confidence interval.

Figure 12 shows the Tukey statistical analysis output. There was not a statistical difference between the overall degradation among the various molar ratios. The same general degradation occurred for each molar ratio.

#### **Figure 12: Tukey pairwise comparison of overall degradation**

Multiple Comparison of Means - Tukey HSD, FWER=0.05 group1 group2 meandiff p-adj lower upper reject Fifty One hundred 0.0845 0.5585 -0.0963 0.2653 False Fifty One thousand -0.0053 0.9 -0.186 0.1755 False Fifty Two fifty 0.0419 0.9 -0.1389 0.2227 False Five hundred One hundred -0.0104 0.9 -0.1912 0.1704 False Five hundred One thousand -0.1002 0.4134 -0.281 0.0806 False Five hundred Two fifty -0.053 0.8531 -0.2338 0.1278 False One hundred One thousand -0.0898 0.5093 -0.2706 0.091 False One hundred Two fifty -0.0426 0.9 -0.2234 0.1382 False One thousand Iwo fifty 0.0472 0.9 -0.1336 0.2279 False 

Figure 13 shows the Tukey statistical analysis output. There was a statistical difference of rate constants between the 500:1 ratio and the 50 and 1000 ratios. A similar reaction rate can be reached at the 100:1 ratio as the 250 and 500:1 ratios while utilizing  $less H<sub>2</sub>O<sub>2</sub>$ .

Multiple Comparison of Means - Tukey HSD, FWER=0.05 group1 group2 meandiff p-adj lower upper reject Fifty One thousand 0.0233 0.9 -0.0959 0.1425 False Fifty Two fifty 0.0867 0.1942 -0.0325 0.2059 False<br>Five hundred One hundred -0.07 0.3615 -0.1892 0.0492 False Five hundred One thousand -0.1233 0.0419 -0.2425 -0.0041 True Five hundred Two fifty -0.06 0.4978 -0.1792 0.0592 False One hundred One thousand -0.0533 0.5924 -0.1725 0.0659 False One thousand Iwo fifty 0.0633 0.451 -0.0559 0.1825 False 

**Figure 13: Tukey pairwise comparison of rate constants**

Figure 14 shows the MS chromatogram of potential reaction byproducts at time 17.285. There are notable peaks at 259 and 260 amu. The peak at 260 amu may be due to the addition of two oxygen to BPA (Dr. D. Felker, personal correspondence, December 2020).



### **Figure 14 MS Chromatogram at time 17.258**

Figure 15 shows the MS chromatogram of potential reaction byproducts at time 10.311. There is a notable peak at 253 amu. This may be due to the addition of CN to BPA (Dr. D. Felker, personal correspondence, December 2020). Both chromatograms had significant peaks that could not be determined with previous research.

#### MSD1 SPC, time=10.611 of Z:\HPLC\_MS\DATA\20200917A\_DLF\_BPA\_ACN 2020-09-17 10-07-55\1DG-0301.D ES-API, Pos, Scan, Fr 269.0  $100 -$ Max: 1953  $90 -$ 80  $70 -$ 255.0 265.0 60 227.0  $50\,$ 229.0 221.0 216.0 251.0 217  $^{22}$  $\circ$  $-223.0$ 233.0 239.0 241.2 249.0  $40 -$ 287 257.0  $\mathbf{Q}$ 235 263.0 219.0  $-218.0$ o 231.0 243.0 222.0 259  $30<sub>o</sub>$  $-226.0$ 234.0 228.2 220.0  $-230.0$ 232.2  $-242.0$ 236.2 250.2 256.0 268.0 248.0 266.2 237.8 240.2 244.2 246.2 257.8 262.2 260.2 264.0  $20 10 220$  $230$  $250$  $270$  m/z 240 260

### **Figure 15 MS Chromatogram at time 10.611**

#### **V. Conclusions and Recommendations**

#### **5.1 Chapter Overview**

This chapter evaluates future research possibilities and recommendations for improvement.

#### **5.2 Research Conclusions**

Statistical analysis did not show a statistical difference between the overall degradation of any of the molar ratios. There was a statistical difference of the degradation rate constants between the 500:1 ratio and the 50 and 1000:1 ratios. The data suggests that peroxide-limited reactions and radical scavenging impacted BPA degradation. The reactions of the lower molar ratios, 50, 100, and 250:1, were limited by the amount of  $H_2O_2$ . Less  $H_2O_2$  in the solution resulted in fewer radicals produced, subsequently reducing radical-BPA reactions and inhibiting BPA degradation. Due to the highly reactive nature of hydroxyl radicals, they indiscriminately react with other compounds. More favorable thermodynamic reactions facilitate radical scavenging, also inhibiting BPA degradation.

#### **5.3 Research Significance**

This research provided additional data that may continue to improve the technology that will enable an optimal water treatment process for contaminant degradation. This study was the first UV LED  $H_2O_2$  AOP trial that investigated BPA degradation kinetics under the parameters utilized. This research illustrated that BPA degradation occurs utilizing UV LED and  $H_2O_2$  and that a molar ratio of 100:1 may

obtain the same rate constant as the 250 and 500:1 ratios with the benefit of using less  $H<sub>2</sub>O<sub>2</sub>$ .

### **5.4 Recommendations for Future Research**

Additional research trials centered around the 100:1 molar ratio may narrow down the optimal ratio for degradation and rate constant. Additional trials will also increase the sample size, lending itself to a stronger statistical analysis. Implementing LED testing will ensure that the LEDs are working consistently across each experiment. Future studies should also consider more powerful LEDs, the effect of co-contaminants, and larger scale testing.



## **Appendix A. Data for 29 March – 0:1 ratio with 10.048 mg/L BPA solution**



## **Appendix B. Data for 14 Aug, Exp 1. – 50:1 ratio with 10.05268 mg/L BPA solution**



## **Appendix C. Data for 14 Aug, Exp 2. – 50:1 ratio with 10.05268 mg/L BPA solution**



# **Appendix D. Data for 28 Aug, Exp. 1 – 50:1 ratio with 10.051068 mg/L BPA solution**



## **Appendix E. Data for 5 June – 100:1 ratio with 10.044 mg/L BPA solution**



## **Appendix F. Data for 19 June – 100:1 ratio with 10.05888 mg/L BPA solution**



## **Appendix G. Data for 26 June – 100:1 ratio with 10.043 mg/L BPA solution**

<b>Sample</b>	Concentration	<b>Time</b>	<b>RT</b>	Peak	Concentration		
	%	(min)	(min)	Area	mg/L		
<b>Blank</b>	$\mathbf 0$		$\mathbf 0$	$\mathbf 0$	0		
<b>Standard</b>	10		1.086	17.9	1.0051068		
<b>Standard</b>	20		1.088	42.3	2.0102136		
<b>Standard</b>	40		1.088	82.3	4.0204272		
<b>Standard</b>	60		1.086	120	6.0306408		
<b>Standard</b>	80		1.087	169.7	8.0408544		
<b>Standard</b>	100		1.087	201.8	10.051068		
<b>Control</b>						Cn/CO	Average
							<b>Control</b>
C1	89.5943	$\mathbf 0$	1.087	183.8	9.005184017	0.895943	9.0693845
C <sub>2</sub>	89.8859	10	1.086	184.4	9.034492931	0.898859	
C <sub>3</sub>	91.1009	20	1.09	186.9	9.156613408	0.911009	
C <sub>4</sub>	90.8093	30	1.085	186.3	9.127304493	0.908093	
C <sub>5</sub>	90.2747	40	1.087	185.2	9.073571484	0.902747	
C6	89.3513	50	1.085	183.3	8.980759922	0.893513	
C <sub>7</sub>	90.6149	60	1.087	185.9	9.107765217	0.906149	
<b>Test</b>						Cn/CO	
R1	85.7549	$\mathbf 0$	1.089	175.9	8.619283312	0.9503714	
R <sub>2</sub>	41.8205	$\overline{2}$	1.086	85.5	4.203406893	0.4634721	
R <sub>3</sub>	33.5099	$\overline{4}$	1.087	68.4	3.368102836	0.3713706	
<b>R4</b>	25.9283	6	1.086	52.8	2.606071064	0.2873482	
<b>R5</b>	19.0757	10	1.092	38.7	1.917311578	0.2114048	
R <sub>6</sub>	15.7223	15	1.086	31.8	1.580259064	0.174241	
<b>R7</b>	16.4999	20	1.087	33.4	1.658416169	0.1828587	
R <sub>8</sub>	17.5205	25	1.09	35.5	1.760997369	0.1941694	
R <sub>9</sub>	16.6457	35	1.089	33.7	1.673070626	0.1844746	
<b>R10</b>	15.0419	45	1.089	30.4	1.511871597	0.1667006	
R11	15.6737	60	1.088	31.7	1.575374245	0.1737024	

**Appendix H. Data for 28 Aug, Exp. 2 – 250:1 ratio with 10.051068 mg/L BPA solution**



# **Appendix I. Data for 3 Sept, Exp. 1 – 250:1 ratio with 10.046889 mg/L BPA solution**



# **Appendix J. Data for 3 Sept, Exp. 2 – 250:1 ratio with 10.046889 mg/L BPA solution**



# **Appendix K. Data for 1 July – 500:1 ratio with 10.0432 mg/L BPA solution**



# **Appendix L. Data for 10 July – 500:1 ratio with 10.04772 mg/L BPA solution**



# **Appendix M. Data for 17 July – 500:1 ratio with 10.043578 mg/L BPA solution**



# **Appendix N. Data for 24 July – 1000:1 ratio with 10.0444 mg/L BPA solution**



# **Appendix O. Data for 31 July – 1000:1 ratio with 10.049332 mg/L BPA solution**



# **Appendix P. Data for 7 Aug – 1000:1 ratio with 10.051849 mg/L BPA solution**





**Amps AK 18 Start <b>K** 18 End





**AK 19 Start <b>K** 19 End















**Appendix V. MATLAB Model – 100:1 ratio, 5 Jun**





**Appendix X. MATLAB Model – 100:1 ratio, 26 Jun**



**Appendix Y. MATLAB Model – 250:1 ratio, 28 Aug**


**Appendix Z. MATLAB Model – 250:1 ratio, 3 Sept Exp. 1**



**Appendix AA. MATLAB Model – 250:1 ratio, 3 Sept Exp. 2**



**Appendix BB. MATLAB Model – 500:1 ratio, 1 July**





**Appendix CC. MATLAB Model – 500:1 ratio, 10 July**





**Appendix EE. MATLAB Model – 1000:1 ratio, 24 July**





**Appendix FF. MATLAB Model – 1000:1 ratio, 31 July**





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