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Richard A. Schilke

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HEXAVALENT CHROMIUM DISSOCIATION FROM OVERSPRAY PARTICLES INTO FLUID FOR THREE AIRCRAFT PRIMERS

THESIS

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AFIT/GEE/ENV/02M-12

DEPARTMENT OF THE AIR FORCE AIR UNIVERSITY AIR FORCE INSTITUTE OF TECHNOLOGY

Wright-Patterson Air Force Base, Ohio

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THESIS

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In Partial Fulfillment of the Requirements for the

Degree of Master of Science in Engineering and Environmental Management

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March 2002

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Richard A. Schilke

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Abstract

The Department of Defense and industry use chromate-containing primer paints extensively to inhibit corrosion on metal assets. Chromate, a primer pigment, provides excellent corrosion inhibition, but contains hexavalent chromium (Ct^6) , a human carcinogen. There is no reliable epidemiological evidence of increased lung cancer incidence among painters potentially exposed to primer overspray particles. Using bioaerosol impingers, overspray particles from three different primers (solvent-borne epoxy, water-borne epoxy, and solvent-borne polyurethane) were collected into water to test the hypothesis that the paint matrix influences Cr^{6+} release into water. This collection method is intended to simulate Cr^{6+} release from paint particles into lung fluid. Collected particles were allowed to reside in the water for ¹ and 24 hours after which the particles were separated from the water by centrifugation. Supernatant water was then tested for dissolved $[Cr^{6+}]$. The mean fractions of Cr^{6+} released into the water after 1 and 24 hours for each primer (95% confidence) were: $70 \pm 5%$ and $85 \pm 5%$ (solvent epoxy), $74 \pm 4%$ and 84 \pm 4% (water epoxy), and 94 \pm 3% and 95 \pm 2% (polyurethane). The epoxy primers demonstrated a range of 24-hour Cr^{6+} release from complete (100%) dissociation to as low as 33% for the solvent epoxy, and 48% for the water epoxy. Correlations between the distribution of Cr^{6+} with particle size and % Cr^{6+} dissociated from each sample indicate that particles $\leq 5 \mu$ m release a larger fraction of their Cr⁶⁺ during the first 24 hours versus particles $> 5 \mu$ m.

HEXAVALENT CHROMIUM DISSOCIATION FROM OVERSPRAY PARTICLES INTO FLUID FOR THREE AIRCRAFT PRIMERS

I. Introduction

Primer Paint Applications

Chromate-containing primer paints are widely used throughout the Department of Defense (DOD) and industry to inhibit corrosion on metal assets that are regularly exposed to corrosive environmental effects. The United States Navy (USN), Marine Corps (USMC), Army (USA), and Air Force (USAF) are large consumers of these chromate-containing primers for ship, aircraft, vehicle, and weapons coating systems. Primers coat the metal skin of an asset providing an adhesive coating for topcoat paints and long-term corrosion protection. Some benefits of corrosion protection include: reduced maintenance, improved structural integrity, and longer service-life. Chromate salts, such as strontium chromate $(SrCrO₄)$, barium chromate $(BaCrO₄)$, or zinc chromate $(ZnCrO₄)$, serve as the primary ingredient in primers to protect metal surfaces from corrosion. Chromate-containing primer paints provide superior corrosion protection over any other primer paints (NDCEE, 1998b). However, chromate contains hexavalent chromium (Cr^{6+}) , a heavily regulated human carcinogen.

Primer paint performance requirements are dictated by military (MIL-P) and federal (TT-P) specifications. Frequently used DOD chromate-containing primer specifications for ship and aerospace applications are shown in Table 1. $SrCrO₄$ is the most common form of chromate in these specifications.

Specification $#$	Primer Type
$ML-P-23377G$	Solvent-borne epoxy polyamide
$MIL-P-85582B$	Water-borne epoxy polyamide
$TT-P-2760A$	Solvent-borne elastomeric polyurethane

Table 1. Prominent Chromate-containing Military Primers

Chromium Carcinogenicity

Chromium in the trivalent form (Cr^{3+}) is an essential mineral for human health. Hexavalent chromium (Cr^{6+}) , however, has been shown to be carcinogenic to both animals and humans. Based on evidence from animal toxicology and human epidemiology studies, several agencies have declared Cr^{6+} a known human carcinogen due to its potential to cause DNA damage. These agencies include: the Agency for Toxic Substances and Disease Registry (ATSDR, 1990), the International Agency for Research on Cancer (IARC, 1990), the Occupational Safety and Health Administration (OSHA, 1996), the National Institute for Occupational Safety and Health (NIOSH, 1997), and the American Conference of Governmental Industrial Hygienists (ACGIH, 2001). While the intracellular mechanism of DNA damage is not well understood, the idea that Cr^{6+} facilitates the DNA damage is well accepted (Sugden & Stearns, 2000; Jones, 1990).

Occupational Chromium Exposure

Prolonged inhalation exposure to high doses of Cr^{6+} is a significant risk factor for lung cancer and can cause other non-carcinogenic respiratory effects such as nasal ulceration (IARC, 1990; Jones, 1990). Epidemiology and animal studies have shown the genotoxic potential of Cr^{6+} when it is readily available for absorption into cells in amounts that exceed the body's capacity to reduce Cr^{6+} to the less hazardous Cr^{3+} [see Jones (1990) for a review]. Cr^{6+} carcinogenic effects due to chronic inhalation exposure

are well documented by case studies of workers in such industries as chromium manufacturing, chromium plating, leather tanning, stainless steel welding, and chromate pigment production where exposure to Cr^{6+} is from acid mists, fumes, or dusts (IARC, 1990; Langard, 1990; O'Flaherty and Radike, 1991). However, current epidemiology studies do not include credible evidence of similar effects from chromate exposure during painting operations. Also, previous animal studies do not accurately represent exposure pathways seen in painting operations. Painters are exposed to airborne paint particles containing $SrCrO₄$ that is predominantly in solid form (LaPuma et al., 2001). The $SrCrO₄$ is contained in the paint matrix, which primarily consists of resin and organic solvents or, for water-borne primers, a combination of resin, water, and solvents. This paint matrix may inhibit Cr^{6+} availability even if paint particles are deposited into the lung fluid. Differences in composition between paint particles and other chromatebearing particulates may explain the lack of a clear connection between chromatecontaining primer painting and lung cancer incidence. These factors suggest that the bioavailability of Cr^{6+} from inhaled paint overspray particles differs from that due to inhalation of particles found in other occupations.

Exposure Standards

In the United States, OSHA is charged with setting workplace exposure limits, known as permissible exposure limits (PEL), for hazardous substances. OSHA considers both worker health and feasibility when setting limits for industry (OSHA, 1996). The agency sometimes limits inhalation hazards using ceiling PELs that limit the maximum substance concentration in the air. The current OSHA ceiling for chromate (as $CrO₃$) is 0.1 mg/m^3 (29 Code of Federal Regulations 1910.1000, Table Z-2). In 1993, OSHA

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received a petition from the Oil, Chemical, and Atomic Workers International Union (OCAW) and the Public Citizen's Health Research Group (HRG) to issue an emergency temporary standard (ETS) for Cr^{6+} compounds of 0.0005 mg/m³ as an 8-hour timeweighted average (TWA) [OSHA, 1996]. This standard is the ACGIH recommended Threshold Limit Value (TLV) for SrCr04 (ACGIH, 2001). The petition, while denied, provided the impetus for a proposed rule pending further OSHA investigation (OSHA, 1996; 2000). If adopted, the limit would virtually ban military and industrial use of chromate-containing primer paints due to the difficulty in meeting such a low standard, even with respirator protection. Furthermore, if Cr^{6+} bioavailability from primer overspray particles is much lower than from particles in other industrial exposures, the proposed standard may be unnecessarily low for painting operations.

Thesis Objective

Previous research investigating Cr^{6+} bioavailability in painting operations suggests that the paint matrix hinders Cr^{6+} dissociation from primer particles into a simulated lung fluid (SLF) [Kauth, 2001]. The research focused on the solvent-borne epoxy polyamide (MIL-P-23377G) specification only. This study, which is a follow-up to the Kauth study, has three primary objectives:

- 1) Observe the influence of particle residence time in fluid on the quantity of Cr^{6+} dissociated from chromate-containing primer overspray particles
- 2) Compare the solvent-borne epoxy (MIL-P-23377G), water-borne epoxy (MIL-P-85582B), and solvent-borne polyurethane (TT-P-2760) primers to observe differences in Cr^{6+} dissociation
- 3) Quantitatively relate particle size to Cr^{6+} dissociation from primer particles into fluid

II. Literature Review

Overview

Aircraft painters are potentially exposed to paint particles via inhalation of overspray. Actual exposure can vary greatly over time due to many environmental, physiological, and chemical influences. In addition to examining existing epidemiology and animal studies, assessing a painter's risk due to Cr^{6+} exposure from primer paints requires an understanding of the fundamental mechanisms that determine Cr^{6+} bioavailability. Cr^{6+} bioavailability to painters depends on complex interactions related to such factors as: paint composition, lung particle deposition and clearance mechanisms, physiological Cr^{6+} reduction, particle inhalation dynamics, the size and composition of inhaled overspray particles, and $Cr⁶⁺$ dissociation from inhaled paint particles once in the lung fluid. After establishing a historical perspective regarding $Cr⁶⁺$ bioavailability and carcinogenicity, this chapter discusses the significance and interaction of these six factors as they apply to better understanding a painter's risk of Cr^{6+} exposure from chromatecontaining primer overspray particles.

Epidemiology/Pathology/Animal Studies

Epidemiology, human pathology, and animal studies provide abundant evidence of the inherent carcinogenicity of Cr^{6+} (IARC, 1990). In order to damage DNA, Cr^{6+} must first be made available to the target (lung) cell. Studies indicate the importance of the chemical and physical form of a Cr^{6+} compound in determining bioavailability. Evidence suggests that only certain Cr^{6+} -containing compounds have demonstrated the ability to cause lung cancer and that there is an exposure threshold below which carcinogenic effects are not seen. (Ishikawa, et al., 1994; Jones, 1990; Mancuso, 1975)

Since Newman (1890) reported the first known association of cancer with a worker's exposure to chromium pigments, numerous cohort studies report increased cancer risks due to chronic exposure to certain $Cr⁶⁺$ -containing compounds (IARC, 1990). Elevated lung cancer rates are observed primarily in the production of chromium compounds from chromite ore, chromate pigment production, chromium electroplating, and stainless steel welding (OSHA, 1996; IARC, 1990). These processes generate Cr^{6+} containing compounds in the form of a dust, fume, or acid mist. Chromium electroplating, for example, generates acid mist containing chromium trioxide (IARC, 1990). Based on a review of epidemiological studies conducted on workers in these industries, Langard (1990) concluded that exposure to Cr^{6+} as chromates, dichromates, or chromic trioxide is responsible for increased lung cancer risk. Langard et al. (1990) found only weak evidence of lung cancer risk in chromium ferroalloy workers. Chromium ferroalloy production exposes workers to chromium compounds consisting primarily of Cr^{3+} and very limited Cr^{6+} . Only one author (Mancuso, 1975; 1997) claims a carcinogenic potential for Cr^{3+} . Thus, evidence strongly implicates inhalation of Cr^{6+} containing compounds, such as chromate, as the primary Cr-related lung cancer hazard.

Multiple studies indicate the importance of chromate dosage and bioavailability in assessing lung cancer risk from Cr^{6+} exposure. A change in processes, around 1960, to eliminate high levels of exposure to slightly water-soluble calcium chromate led to a significant reduction, if not elimination, of excess lung cancer risk in such industries as chromite ore processing and chromate pigment production (Aw, 1997; Jones, 1990). Steinhoff et al. (1986) found evidence of a Cr^{6+} carcinogenic threshold in rats after intratracheal installation of various doses of sodium dichromate. 14 of 80 rats receiving a

single dose of 1.25 mg/kg presented with one or more lung tumors, but no tumors were seen in 80 rats dosed with the same concentration spread over five days (0.25 mg/kg/day). One pathology study based on autopsies of 13 chromate compound production workers found the lung tissue Cr burden was generally much higher in subjects with lung tumors $(40 - 15,800 \text{ µg/g})$ than in those without $(8-28 \text{ µg/g})$ [Ishikawa, et al., 1994]. These studies, among others (Mancuso, 1975; Axelsson et al., 1980; Korallus et al., Bidstrup and Davies, 1986), suggest that a threshold dose exists for Cr^{6+} lung carcinogenicity, and imply the importance of Cr^{6+} concentration in the lung fluid. Finally, a cohort study of male chromate pigment workers producing several Cr^{6+} containing compounds, including $SrCrO₄$, found no excess risk of lung cancer (Kano et al., 1993). The study proposed several possible explanations for the results, including: improved industrial hygiene practices, lower carcinogenicity of some Cr^{6+} compounds, work environment concentrations below a dose-response threshold, or a dependence of carcinogenicity on the chemical form of the compound.

Epidemiological evidence of carcinogenic risk from chromate-containing paint operations is weak. One study (Dalager et al., 1980) of 977 male aircraft painters using zinc chromate-containing paint found an excess of respiratory cancer (21 observed, 11.4 expected). Unfortunately, this study did not account for smoking and, according to the authors, smoking among painters is more prevalent than in the general population. Another study (Alexander et al., 1996) of 2,429 chromate-exposed aerospace workers found no excess of lung cancer in 1,064 spray painters (6 observed, 11.1 expected). The authors suggest "incorporation of the chromate into the paint matrix may render it less biologically active." Further support for this statement is offered by the fact that sanders

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in this study who were exposed to the same compounds, but in potentially less encapsulated dust particles, showed an excess of lung cancer.

Documented animal studies demonstrate that the solubility of Cr^{6+} -containing compounds is a key factor in determining carcinogenic potential. Animal studies indicate that the moderately soluble zinc, calcium, and strontium chromate salts have much greater carcinogenic potential than the highly soluble sodium, potassium, and ammonium chromates (Hathaway, 1989; Gibb and Chen, 1989). Sodium dichromate, installed in rat trachea in the Steinhoff et al. (1986) study, is highly soluble. These authors conclude that "easily soluble chromates signify a relatively small risk of a carcinogenic effect and then only when high doses are absorbed over a very long period", and also that the chronic irritant effect associated with repeated high doses probably served to promote pulmonary tumors in the rats. It seems that while highly soluble Cr^{6+} compounds might temporarily produce higher available Cr^{6+} concentrations in the lung, their Cr^{6+} is chemically reduced and cleared more rapidly (Gad, 1989; O'Flaherty and Radike, 1991). To the contrary, insoluble Cr^{6+} compounds, such as lead chromate, fail to produce high concentrations of $Cr⁶⁺$ in the lung. Thus, the carcinogenic potential appears greatest for moderately soluble Cr^{6+} compounds, which possess the ability to release sufficient Cr^{6+} *and* to reside in the lung fluid for a sufficient time.

Animal studies demonstrate that some Cr^{6+} -containing compounds are genotoxic, but do not provide information about the relationship between exposure and carcinogenic effects. The majority of existing animal studies used implantation of solid chromate compounds directly into target tissues (e.g. intrabronchial, intratracheal) [IARC, 1990]. While implantation studies demonstrate a carcinogenic potential for Cr^{6+} -containing

compounds, inhalation exposure of animals to these compounds has not shown a clear link to pulmonary tumors (IARC, 1990; Langard, 1988). IARC reports only one animal inhalation study (Nettesheim et al., 1971) that shows a significant incidence of lung tumors. That study exposed mice to calcium chromate dust.

ACGIH set its lower TLV based primarily on a study by Levy et al. (1986) in which rats were dosed through intrabronchial implantation of cholesterol pellets containing various chromate compounds (ACGIH, 2001). After two years of observation, the study found that groups exposed to strontium chromate and zinc chromate showed a statistically significant increase in bronchial tumors. While the study effectively demonstrates the carcinogenicity of these compounds, the implantation exaggerates exposure concentration, negates the effects of respiratory filtering and clearance mechanisms, and does not present the compound in a matrix similar to paint.

Primer Paint Composition

Primer paints are complex mixtures that are tailored to meet the coating needs of various types of metal and anticipated exposure environments. The primary paint constituents are the pigment, the vehicle, and the solvents (USAF, 2001). Pigments are mostly insoluble and provide several benefits including color and corrosion- inhibition. The three primers used in this study (Table 1) all use Cr^{6+} -containing SrCrO₄ pigment as the corrosion inhibitor (USAF, 2001; USN, 2001). The vehicle, or liquid portion of the coating, enables paint delivery, adhesion, flexibility, durability, and chemical resistance. The vehicle contains both volatile and non-volatile components. Volatiles consist primarily of a solvent mixture that thins the paint for delivery to a metal surface, and enables smoothing and binding of the paint coating. Resins comprise the majority of

non-volatiles and act as binding agents to link together pigment granules and a potential host of secondary components depending on the intended application. Epoxy and Polyurethane primers cure by chemical cross-linking rather than dry by evaporation (USAF, 2001). Cross-links form during curing ofthe paint matrix to establish the paint film and bind the chromate (Munger, 1984). If the paint subsequently cracks or is scratched, chromate ions are electrochemically attracted to the exposed metal (anode) and prevent oxidation of the metal by reforming the protective barrier (Miller, 1979).

 $\text{Def}_{\mathcal{B}}$ Incorporated supplies the military with large amounts of chromatecontaining solvent-borne epoxy, water-borne epoxy, and solvent-borne polyurethane primers. For this reason, and the desire to maintain manufacturer consistency between paints, Deft[®] primers were selected exclusively for this study. Deft[®] Material Safety Data Sheet (MSDS) excerpts for the three specifications used in this study are included in Appendices A, B, and C. All of these primers are two-component mixtures consisting of a pigment- and resin-containing base (Component A) and a curing agent catalyst (Component B). The water-borne primer requires addition of water as a reducing component. Table 2 summarizes the primer mix ratios and Table 3 summarizes the MSDS-listed contents of the Deft[®] primers.

Primer	Base	Catalyst	H_2O	
Solvent-borne epoxy	75.0 %	25.0%	N/A	
Nater-borne epoxy	28.6 %	14.3 $\%$	57 1 $\%$	
Solvent-borne polyurethane	50.0 %	50.0 %	N/A	

Table 2. Primer Component Mix Ratios. Shown as a % volume in the final mixture.

Solvent-Borne Epoxy		Water-Borne Epoxy		Polyurethane	
Constituent	$\overline{\%}$ Wt	Constituent	% Wt	Constituent	% Wt
Benzene, 1-Chloro-4 Trifluoromethyl	< 4.1	sec-Butyl Alcohol	8.4	Isobutyl Alcohol	${}< 0.1$
Benzene, 1-Chloro-4 Trifluoromethyl	< 0.1	C8 & 10 Aromatic Hydrocarbon	${}< 0.3$	Ethyl 3-Ethoxypropionate	5.9
n-Butyl Acetate	< 4.1			n-Butyl Acetate	< 3.0
Methyl n-Propyl Ketone	$\overline{20.3}$			Methyl Ethyl Ketone	< 3.0
Strontium Chromate	20.3	Strontium Chromate	9,9	Strontium Chromate	11.9
Aromatic Hydrocarbon	< 0.8			2,4-Pentanedione	< 3.0
Xylene	${}_{0.08}$			Xylene	< 0.6
1, 2, 4 Trimethylbenzene	${}_{0.8}$			Dibutyltin Dilaurate	< 0.1
Cumene	${}< 0.1$			Dispersion Aid	${}< 0.6$
1, 3, 5 Trimethylbenzene	${}_{0.8}$			Anti-float Agent	${}< 0.6$
Diethylbenzene	< 0.8			Ethyl Benzene	< 0.1
Ethyl Benzene	${}< 0.1$				
n-Methylpyrrolidone	< 0.8				
Polyamide Resin	≥ 36.3	Polyamide Resin	≥ 25.3	Oil-free Polyester	≥ 30.7
Aliphatic Amine	< 3.0	Nitroethane	4.4	Polymeric Hexamethylene Diisocyanate	22.4
sec-Butyl Alcohol	5.6			Methyl Isobutyl	8.1
Aromatic Hydrocarbon	${}< 0.2$			n-Butyl Acetate	< 2.0
Xylene	${}< 0.02$			Methyl Ethyl Ketone	8.1
1, 2, 4 Trimethylbenzene	${}< 0.2$	De-ionized Water	51.7		
Cumene	${}< 0.02$				
1, 3, 5 Trimethylbenzene	${}< 0.2$				
Diethylbenzene	${}< 0.02$				
Ethyl Benzene	${}< 0.02$				
Amino Silane Ester	< 0.2				
Epoxy Resin Hardener	≤ 1.0				

Table 3. Comparison of Deft® Mixed Primer Contents (adapted from MSDSs).

Double lines separate components (base||catalyst||water, top to bottom). % Wt **represents the constituent post-mixing percent weight in the mixture.**

Though some portion of chromate pigment dissolves into each primer's volatiles, consisting of solvents or water and solvents, the majority of the chromate remains in solid form. The total mass of $SrCrO₄$ per volume of paint in this study's three primers is approximately: 251,900 mg/L (solvent-borne epoxy), 111,200 mg/L (water-borne

epoxy), and 139,200 mg/L (solvent-borne polyurethane). The solubility limit of $SrCrO₄$ in methyl ethyl ketone (MEK), a solvent representative of the volatiles in the solventborne primers, is 45 mg/L (LaPuma et al., 2001), but in water at 15° C it's 1200 mg/L. Therefore, while a very small portion of chromate actually dissolves into the volatiles, the water-borne epoxy volatiles (77% water by volume) contain nearly 21 times as much SrCr04 (940 mg/L) as the solvent-borne epoxy and polyurethane volatiles at saturation. Finally, the water-borne primer contains a much larger fraction of volatiles (74% by volume vs. 41% for the solvent epoxy and polyurethane), which are mostly water.

Solvent-borne vs. Waterborne Primers

Solvent-borne paints are preferred for their longer shelf life, shorter dry times, ease of application, and performance for a wide range of metal surfaces and environmental conditions (NDCEE, 1998a), but they release volatile organic compounds (VOCs) to the atmosphere. VOCs accelerate the production of tropospheric ozone, a major contributor to photochemical smog and a human health concern, especially for individuals suffering from respiratory disorders (Godish, 1997). Water-borne primers, such as MIL-P-85582B, have become increasingly available in recent years due to the benefits of their low VOC formulation in complying with more stringent regional tropospheric ozone standards (USEPA, 2000). Although water-borne primer use reduces VOC emissions, and presumably tropospheric ozone, it may increase the carcinogenic risks to painters by delivering Cr^{6+} in a more bioavailable form.

If the primer matrix limits Cr^{6+} dissociation from primer particles such that Cr^{6+} is only available from the chromate dissolved in the volatiles, then increasing the amount of chromate in the volatiles or the ability of the volatiles to transfer Cr^{6+} to the fluid may

increase Cr^{6+} bioavailability. This may occur through an increase in: chromate solubility in the volatile fraction, volatile fraction solubility in lung fluid, or the volatile % volume in the paint mixture. If chromate dissolved in the paint volatiles is the primary source of Cr^{6+} to the lung fluid, the volatile fraction saturation limit and % volume comparisons made in the previous section predict that more Cr^{6+} mass may be released from the waterborne epoxy primer than from either solvent-borne primer. Additionally, the increased solubility of the mostly-water volatile fraction in an aqueous lung fluid compared to that of non-polar solvent volatiles predicts greater Cr^{6+} release from the water-borne primer.

Primer Painting Operations

Primers containing zinc, barium, or strontium chromate are applied to aluminum, magnesium, and their alloys to provide corrosion protection and an adherent layer between the metal and the topcoat (USAF, 2001; USN, 2001). Large-scale spray painting operations typically take place in ventilated painting areas or booths that have a minimum airstream velocity of 100 feet per minute (ACGIH, 1995). To reduce VOC emissions and the amount of coating material lost to overspray, the use of high-volume low-pressure (HVLP) spray guns at nozzle pressure settings between ¹ and 10 pounds per square inch (psi) is becoming the standard for aircraft painters (USAF, 2001). HVLP spray is used to apply very thin coats of primer to the target surface. Air Force and Naval technical manuals (USAF, 2001; USN, 2001) specify desired primer dry coat thickness ranges of:

- 0.6 to 1.8 mils (.0006 to .0018 inches) for the solvent-borne epoxy and waterborne epoxy primers
- 1.0 to 2.0 mils (.0010 to .0020 inches) for the polyurethane primer

Since paint transfer efficiency may be as low as 65% for HVLP and even lower (35-50%) when conventional high-pressure spray guns are used, a portion of the paint becomes

inhalable overspray (USN, 2001; US AF, 2001). Variables such as painting technique, object size, and number and location of individuals painting simultaneously contribute to varying inhalation exposure potential. Since ventilation systems and personal respirators can be improperly used or overwhelmed, the opportunity for chronic worker exposure to chromate-containing overspray particles remains an important concern.

Particle Deposition and Clearance Mechanisms in the Lung

Inhalation is the primary route of painter exposure to aerosolized paint particles. When particles are inhaled, they deposit throughout the respiratory system with a distribution that depends on many factors but is strongly related to particle aerodynamic diameter. Some other important parameters are: airway shape, structure, and diameter; air flow rate; air velocity; route of entry (nasal or oral); particle size, solubility, and hygroscopicity (Seinfeld, 1986; Phalen, 1984). These factors combine to force particle deposition via interception, impaction, sedimentation, or diffusion.

Aerodynamic diameter (d_{ae}) is defined as the diameter of a unit density (1 g/cm³) sphere having the same terminal settling velocity as the particle under study (Seinfeld, 1986). Assuming spherical particles, terminal settling velocity (v_t) for an aerosol particle is defined by Stokes' Law as (Clark, 1996):

$$
v_t = \frac{C_c^2 r_p d_p^2}{18 \cdot \mu} \cdot g \tag{1}
$$

where: C_c = Cunningham Slip Correction factor (unitless) [diameterdependent]

 ρ_p = particle density (g/cm³)

- d_p = particle diameter (cm)
- μ = dynamic viscosity of air (g/cm·s) [temperature-dependent]
- $g =$ acceleration due to gravity (cm/s²)

 d_{ae} is determined by substituting this v_t and solving equation 1 for d_p when $p_p = 1$ g/cm³:

$$
d_{ae} = \sqrt{\frac{v_t \cdot (18 \cdot \mu)}{C_c \cdot \left(1 \frac{g}{cm^3}\right) \cdot g}}
$$
(2)

The relationship between particle diameter (d_p) , particle density (ρ_p) , and d_{ae} is easily seen if the right-hand side of equation 1 is substituted into equation 2 for v_t and constants are cancelled:

$$
d_{ae} = \sqrt{\frac{?_{p} \cdot d_{p}^{2}}{\left(1 - \frac{g}{cm^{3}}\right)}}
$$
(3)

Thus, d_p and p_p directly influence d_{ae} , which affects how a particle is inhaled and deposited in the respiratory tract.

The respiratory system contains two main regions called the conducting zone and the respiratory zone (Figures 1 & 2). The conducting zone consists of the oral and nasal airways, pharynx, larynx, trachea, bronchi, and bronchioles, and can be subdivided into the head and conductive airway regions. During inhalation, the upper conducting zone filters large particles, and pre-warms and humidifies air prior to passage through the trachea and bronchi. The respiratory zone, also called the pulmonary region, includes the respiratory bronchioles and alveoli (Fox, 1999; Seinfeld, 1986) and is the area of oxygen and carbon dioxide gas exchange with the blood. Gas is primarily exchanged in the alveoli, which provide about 60 to 80 $m²$ of gas exchange surface area in the lung (Fox, 1999). The respiratory system (except the alveoli) is lined with a layer of mucus atop hair- like cilia that project from the walls of the airways. Cilia protrude from lung cells and exist in a watery serous fluid that is covered by the mucus layer. Cilia transport the

mucus layer upward at a rate of ¹ to 2 cm per minute (Fox, 1999) by beating in a coordinated stroking motion. This process is known as mucociliary escalation.

Figure 1. Human Respiratory Tract Schematic Diagram (Hinds, 1982:17)

Figure 2. Conducting and Respiratory Zones (Fox, 1999:484)

Mucociliary escalation of deposited particles is the primary means of particle removal in the conducting zone. Inertial impaction is most prevalent in the conducting zone and accounts for the greatest deposition by mass (Miller et al., 1979). Air velocity, greatest after entering the nostril, gradually slows as the bronchi bifurcate (divide) 19 to 21 times prior to reaching the terminal bronchioles. Due to inertia, most particles with d_{ae} larger than $5 \mu m$ tend to maintain their trajectories when the airway changes direction causing them to impact the mucus lining of the nasal cavity or bronchi walls (Miller et al., 1979). Impaction, interception, sedimentation, and diffusion continue to filter smaller and smaller particles as air descends toward the terminal bronchioles. Particles captured by the mucus lining in the bronchi are transported up the bronchial tree to the pharynx by mucociliary escalation. Mucus and trapped particles are then swallowed or expectorated (Fox, 1999). Mucociliary escalation clears the conducting zone rapidly, removing most trapped particles within 24 hours of inhalation (Lippmann and Albert, 1969; Stahlhofen etal, 1980).

Some particles with d_{ae} less than 5 μ m can navigate past the conducting zone to the respiratory zone (Chan and Lippmann, 1980). The lack ofmucus lining and cilia in the alveoli prevents mucociliary escalation, which increases clearance time and, thus, the potential for health effects (Phalen, 1984). Particles that reach the alveoli are predominantly removed by phagocytosis, where cells called pulmonary alveolar macrophage (PAM) engulf particles and enzymatically break them down.

At inhalation rates of approximately 30 L/min (moderate exercise), inertial impaction in the upper respiratory system removes almost all particles with d_{ae} greater than 10 μ m during nasal inhalation and 15 μ m during oral inhalation (Seinfeld, 1986). At

this flow rate, studies have found that about 20 percent of 1 μ m, 30 percent of 2 μ m, 40 to 50 percent of 3 to 4 μ m, and less than 10 percent of 5 to 10 μ m particles are deposited in the respiratory zone (Chan and Lippmann, 1980; Stahlhofen et al, 1980; Lippman, 1977; Lippman and Altschuler, 1976; Lippmann and Albert, 1969). Figure 3 shows a typical adult male lung particle deposition distribution by region.

Figure 3. Respiratory Particle Deposition Distributions by Region (Health Effects Institute, 1998:2)

Cr6+ Reduction Mechanisms

In addition to lung clearance mechanisms, the human body has a robust capacity for reducing Cr^{6+} to non-carcinogenic Cr^{3+} . Stomach enzymes and acids are able to break down particles that are directly ingested or swallowed after mucociliary escalation, and efficiently reduce Cr^{6+} to Cr^{3+} prior to excretion (DeFlora et al., 1987). Also, enzymes and acids in the lung are capable of reducing Cr^{6+} both inside and outside the epithelial

cells. For example, glutathione, cysteine, and ascorbic acid can reduce Cr^{6+} in the extracelluar environment, and are readily available throughout the lung (Connett and Wetterhahn, 1985). It is known that Cr in the 6+ oxidation state is highly diffusible and able to penetrate into cells (Jones, 1990). Cells are much less permeable to Cr^{3+} , Cr^{4+} (tetravalent), and Cr^{5+} (pentavalent), and resist absorption of these species following extracellular reduction of Cr^{6+} . Reduced species are escalated in the mucous, swallowed, and excreted. If C^{6+} -containing particles reach the respiratory zone, PAM have the ability to enzymatically reduce Cr^{6+} to Cr^{3+} (Petrilli and DeFlora, 1998). In fact, most lung cancers related to Cr^{6+} exposure originate in the nasopharynx and upper airways (conducting zone) [Casarett, 1986].

In order for Cr^{6+} to be absorbed by lung cells it must first saturate the reducing capacity of the lung fluid and concentrate near cell membranes (Jones, 1990). $Cr⁶⁺$ may then be actively transported into cells by mimicking the structure of sulfate and phosphate (Connett and Wetterhahn, 1983). If $Cr⁶⁺$ *is* taken into a cell and then reduced by the cytoplasm, enzymes, or organelles (Connett and Wetterhahn, 1985; Steinhoff et al, 1986; Sugden and Stearns, 2000), the less diffusible reduced species are retained in the cell. It is suspected that these "trapped" reactive intermediates $(Cr^{4+}$ and Cr^{5+}), particularly Cr^{5+} , are responsible for producing oxidative DNA damage (Sugden and Stearns, 2000). Nevertheless, the capacity of respiratory clearance and reduction make it likely that a carcinogenic concentration threshold does exist for inhaled Cr^{6+} . One animal study found that only about 5% of the Cr^{6+} from an inhaled dose was actually absorbed by lung tissue and that most of the Cr^{6+} was excreted in the feces (Visek et al., 1953). Thus, knowing how much Cr^{6+} escapes inhaled paint particles into the lung fluid, and

how quickly it escapes, is critical for assessing lung cancer risk to spray painters from chromate-containing primer overspray.

Paint Overspray and Particle Inhalation Dynamics

The mass and distribution of particles inhaled by a painter depends on worker respiration rate, breathing zone concentration, and breathing zone particle size distribution. Respiration rate typically ranges from about 6 L/min at rest (Fox, 1999) to 30 L/min during moderate exercise (Seinfeld, 1986), and translates to the volume of air inhaled over time. Breathing zone concentration and particle size distribution are influenced by the concentration and size distribution of the overspray, the booth air velocity, and painter orientation to the airflow and paint sources. In painting operations, overspray is produced when paint particles of smaller mass, and therefore less inertia, fail to impact the target surface and become entrained in the local airflow (Carlton and Flynn, 1997a). These localized air currents are mainly created by the nozzle air velocity and booth, or ambient, airflow. Carlton and Flynn (1997b) found that the combination of spray gun nozzle pressure and painter orientation to the booth airstream had the dominant influence on breathing zone distribution. Though that study found no correlation between the spray particle size distribution and the breathing zone distribution, the structure and composition of inhaled overspray particles is influenced by paint spray characteristics.

Paint and Overspray Particle Size Distributions

Overspray particles consisting of paint solids and unevaporated solvents and originate from spray particles produced by paint atomization. The atomized spray distribution is a function of pressure at the nozzle, paint viscosity, and relative air-to-

liquid mass flow rate (Bayvel and Orzechowski, 1993). In addition to these parameters, the $SrCrO₄$ granule size distribution added to the paint by the manufacturer may influence spray particle size and composition. Figure 4 shows a typical $SrCrO₄$ granule size distribution (log scale) in the Deft_® primer mixtures as analyzed by the manufacturer. This distribution contains granules with d_p ranging from .1 μ m to 30 μ m and a geometric mean of about 4 μ m. During spraying, paint from the nozzle is atomized by shearing forces when the surrounding column of discharge air disintegrates the paint liquid into droplets (Bayvel and Orzechowski, 1993). After atomization, the spray particle size distribution may reflect some combination of solvent and epoxy-coated $SrCrO₄$ granules and "smaller" paint particles that do not contain solid SrCrO₄ granules. Overspray originates from this distribution but is weighted toward small particles since, by definition, it consists primarily of the smaller, lower inertia, particles.

Figure 4. Deft® SrCrC>4 Granule Particle Size Distribution in Methanol. Measured on a Malvern Mastersizer Laser and displayed on a log scale.

Overspray Particle Composition

Post-atomization particle composition has three important implications on Cr⁶⁺ bioavailability. Since $SrCrO₄$ is the densest constituent in the primer, particles containing

a greater volume of SrCr04 behave aerodynamically like larger particles and will tend to deposit higher in the respiratory tract. If these particles clear the lungs prior to releasing their Cr^{6+} , Cr^{6+} delivery to the target tissue may be much less than the total mass of Cr^{6+} inhaled in particles. Second, differences in composition associated with particle size may bias the Cr^{6+} deposition distribution in the lung. Previous research suggests that the larger chromate-containing primer paint particles contain significantly more chromate than smaller particles (Novy, 2001; LaPuma et al., 2001). Novy (2001) found that below 10 μ m the mass of Cr⁶⁺ per mass of dry paint decreased linearly with particle mass median aerodynamic diameter (MMAD) [Figure 5]. Third, differences in composition related to the Cr^{6+} bias may cause some particles to release Cr^{6+} more easily than others. Novy (2001) proposed that during atomization, small particles containing mainly resins and solvents may be stripped from larger particles, increasing the relative amount of Cr^{6+} in larger "parent" particles and decreasing it in small "daughter" particles that may not contain solid chromate. If the paint matrix in larger particles holds the chromate within, then Cr^{6+} dissociation may be limited to that from chromate dissolved in unevaporated solvents on parent particle surfaces or in partly soluble daughter particles. Consequently, " smaller" particles may quickly release what little Cr^{6+} they possess while "larger" particles, containing the bulk of the Cr^{6+} , slowly release only a small portion of their Cr^{6+} . **Cr6+ Dissociation**

In order for Cr^{6+} to enter the lung fluid it must dissociate from inhaled paint particles prior to their clearance from the lung. Two previous studies attempted to determine whether particle residence time in lung fluid was related to dissociation (Morgan, 2000; Kauth, 2001). Both studies collected MIL-P-23377G solvent-borne

epoxy overspray particles in SLF using midget impingers. Though results were inconclusive, they indicated some hindrance of Cr^{6+} dissociation from the particles.

Figure 5. Comparison of Mass of Cr per Mass of Dry Paint (Novy, 2001:23)

Influencing Sample Particle Sizes

Understanding any particle size-dependent differences in Cr⁶⁺ dissociation behavior may lead to a more accurate evaluation of Cr^{6+} bioavailability from inhaled primer paint particles, and provide insight into the dissociation mechanisms. Previous data concerning Cr^{6+} dissociation from solvent-borne epoxy particles is limited to collections of only small particle sizes $(< 5 \mu m)$. Kauth (2001) collected particles using a 1.2 L/min impinger flow rate and then characterized the collected particle size distributions using a liquid particle counter. Nearly all the particles collected were in the 1 μ m to 3.5 μ m bins (d_p < 5 μ m). The author suggests that larger particles, containing significantly more SrCrO₄, release a much smaller proportion of their Cr^{6+} . It was noted
that samples with only small particles released the same mass of Cr^{6+} as those with both large and small particles. Thus, there is indication that smaller paint particles release Cr^{6+} more easily than larger paint particles.

In order to understand the relative contributions of different particle sizes to dissociated Cr $^{6+}$, collections must, at a minimum, include a variety of distributions containing significant numbers of particles across the size range of interest. Since paint overspray contains a high concentration of very small particles, the challenge is to collect as many of the larger ($> 5 \mu m$) particles as feasible. Larger particle collection may be achievable by decreasing booth flow and increasing impinger flow rates. Also, varying impinger flow rates should provide some variety of particle size distributions with higher flow rates collecting more large particles.

Research Focus

This research focuses on better understanding Cr^{6+} dissociation from chromatecontaining primer paint overspray particles into fluid as dependent on particle size, time, and matrix composition. First, solvent-borne epoxy overspray is collected. The amount of Cr^{6+} that dissociates from collected particles into fluid after 1 and 24 hours of residence time in the fluid is measured to assess how quickly Cr^{6+} dissociates from overspray particles and whether or not residence time is relevant. Second, the waterborne epoxy and solvent-borne polyurethane primers are analyzed similarly to compare $Cr⁶⁺$ dissociation behavior for all three paints. Primer overspray collection is designed so as to capture a broader range of particle sizes than in previous related research. This may provide added information about the relative contributions from particles of different sizes to the observed fraction of Cr^{6+} that dissolves into water from paint particles.

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III. Methodology

Overview

This chapter provides a description of the methods and equipment used for sample collection, handling, and analysis. The experiment is designed to emulate respirable paint particles inhaled into serous lung fluid so that the fraction of Cr^{6+} dissolving from the particles into the fluid may be determined. This experiment makes the conservative assumption that particles are inhaled, immediately immersed in the watery serous lung fluid layer, and remain there for at least 24 hours. Deposited particles generally float atop the lung's mucous layer so that chromate must dissolve and diffuse through the mucous to the serous fluid before Cr^{6+} is available to lung epithelial cells. This experiment ignores any intervention by the mucous layer or lung clearance and Cr^{6+} reduction mechanisms, and focuses on Cr^{6+} dissociation from particles into water.

Three phases comprise the sampling and analysis plan used to obtain data in this study. First, aerosolized primer paint particles representative of those produced in field painting operations are generated using HVLP spraying equipment in a ventilated paint booth. Second, during spraying, airborne paint particles are trapped and collected in fluid for later analysis. Third, fluid collections are processed and analyzed for particle size distribution and Cr^{6+} dissociation (measured as Cr^{6+} concentration, $[Cr^{6+}]$) over time from particles into the fluid.

Painting Operation

Particle samples were generated in a climate-controlled, ventilated paint booth located at the U. S. Air Force Coatings Technology Integration Office, Wright Patterson Air Force Base, Ohio. The booth is $10' W x 14 L' x 9' H$ and was operated at a 100 fpm

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exhaust face flow rate. Booth temperature $(26.0 \pm 0.6^{\circ} \text{C})$ and humidity $(6.6 \pm 1.1 \%)$ [95 % confidence] were held constant. Paint particles were generated using a DeVilbiss spray gun (product number JGHV-531), fitted with a 46MP air cap. This equipment setup is typical for aircraft painting operations. A "low" and "high" nozzle pressure setting was used for each primer (Table 4) to alter the particle size distribution generated. Prior to each collection, the paint gun nozzle pressure was calibrated using a 46MP test cap and pressure gauge. The same HVLP gun air and paint flow settings were used throughout the study to achieve the spray coarseness and uniformity desired for typical aircraft painting operations.

Primer	Low Pressure (psi)	High Pressure (psi)		
Solvent-borne Epoxy	2.5	8.0		
Water-borne Epoxy		10.0		
Solvent-borne Polyurethane	4.0	8.0		

Table 4. Spray Gun Nozzle Pressure Settings

All paints were mixed and tested for viscosity per the manufacturer's specifications. Selected information for the primers used in this experiment is summarized in Table 5. A type I primer uses standard (i.e. not low-infrared) pigments and Class C or C2 indicate that $SrCrO₄$ is added to the paint. Approximately 0.6 to 1.0 liter (L) of paint was mixed for each session using the component ratios given in Table 2. Paint collection times ranged from 8 to 30 minutes.

Spraying from the HVLP spray gun against a cardboard target generated continuous primer paint overspray. The gun was held in a fixed position 41" above the floor and its trigger was fully depressed with a cable-tie during painting. Nozzle-to-target distance was fixed at 7" (manufacturer and service technical instructions specify 6" to 8"). In order to slow airflow in the vicinity of the samplers and increase the concentration of paint particles, a cardboard baffle $(27"$ W X $25"$ H X $28.5"$ D) was placed around the sampling equipment (Figures $6 \& 7$). The gun sprayed in a direction level to the floor and parallel to the box face. The target was placed at approximately a 20° angle to the center of the spray, allowing the largest particles to impact the target and smaller particles to become entrained in the local airflow as overspray.

Table 5. Paint Data Summary (Deft® Product Information Data Sheets)

	Solvent-borne Epoxy	Water-borne Epoxy	Solvent-borne Polyurethane
Specification	MIL-P-23377G	MIL-P-85582B	TT-P-2760A
Type			
Class	C	C ₂	
Deft Product Code	$02 - Y - 40$	44-GN-72	$09-Y-2$
Batch #'s (Base/Catalyst)	46517/46518	45699/45700	45526/45527
Viscosity spec.* (sec)	21	20	14-24
Induction Time (min)	30	None specified	None specified

"Using a #4 Ford Cup

Figure 6. Paint Booth Setup and Sample Collection Apparatus

Figure 7. Paint Booth Setup Diagram (top down view)

BioSampIer®

Samples were collected using six BioSampler[®] glass impingers manufactured by SKC Incorporated (Figure 8). Designed for collection of bio-aerosols, this device was chosen over the midget impinger due to its high collection efficiency and ability to collect particles at high flow rates. The BioSampIer® uses tangential nozzles to swirl the collection fluid and continuously deposit particles to the surface of the swirling fluid. This means of capturing particles more closely resembles deposition in the lung and eliminates the bubbling of sample air through the fluid that is required by the midget impinger. In order to prevent excessive bubbling, and the resulting loss of particles, the standard midget impinger is limited to low flow rates that tend to collect very small particles (Kauth, 2001). The BioSampler[®] allows the use of higher flow rates while minimizing particle bounce and re-aerosolization. The ability to use higher flow rates

was important in this experiment due to the desire to increase collection of larger overspray particles.

Sampling Plan

Solvent-borne epoxy, water-borne epoxy, and polyurethane overspray samples were collected separately. A total of 117 samples were collected and Table 6 shows the sample allocation by primer type and flow rate. Six BioSamplers collected overspray samples at three different flow rates. Sampler inlet nozzle airflow rates of 2, 5, and 10 L/min enabled collection of a variety of particle size distributions. Higher flow rates increased the capture zone at the sampler inlet and enabled the collection of larger, higher inertia, particles. Samplers were arranged within the baffle as shown in Figure 9. The 1.2 L/min flow rate for positions ¹ and 6 was only used to collect five samples in Teflon® midget impingers for comparison to previous studies. Gilian® GilAir 5 air pumps were connected to each 2 (or 1.2) L/min, and 5 L/min sampler, and airflow from an SKC Air Sampler sonic flow pump (Cat. No. 228-9605) was split to operate each 10 L/min

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sampler. All samplers were calibrated before and after each collection using a Gilibrator Airflow Calibration System #800285/286.

Primer Type	Sampler Flow Rate					
	2 L/min 5 L/min 10 L/min					
Solvent-borne epoxy (in DI only)						
Water-borne epoxy						
Solvent-borne polyurethane						

Table 6. Allocation of Samples by Primer Type and Flow Rate

Figure 9. Sampler Layout (front view)

To better understand the relationship of particle size to Cr^{6+} bioavailability, this study attempted to collect samples with a variety of particle size distributions by varying flow rate. Ideally, the collection data set should consist of samples containing only single particle diameters covering the range of interest. Since no feasible method of isolating overspray particles of single diameters into fluid currently exists, a more realistic depiction of a desirable set of collected distributions is shown in Figure 10. Given the high concentration of very small particles in overspray, the practical limits of impinger flow rates prevent collection ofthe larger particle distributions in Figure 10.

Nevertheless, increasing flow rate enabled a rightward shift in collected particle size distributions as flow rate increased, providing some contrast between distributions.

Figure 10. Desirable Set of Particle Size Distributions for Relating Cr⁶* Dissociation to Particle Size

Background Sampling

Four booth air background collections were conducted to identify and quantify particle and Cr^{6+} background resulting from the paint booth air, collection equipment, and methodology. Background samples were collected: prior to the first paint collection, between the solvent-borne and water-borne epoxy collections, between the water-borne epoxy and polyurethane collections, and after all sampling was complete. These collections provided an estimate of the background contributed by the paint booth air, sample collection vessels, and laboratory handling and equipment. Laboratory air backgrounds were collected prior to the first and after the last booth background measurements. The lab backgrounds sampled presumably "clean" air in order to isolate equipment and process background from that due to the booth air. Procedures for background collection and analysis were identical to those for paint particle samples.

Liquid Particle Counter

The size distribution of particles collected in each de-ionized water (DI) sampler was determined using a Particle Measuring Systems, Inc. Automatic Parenteral Sampling System model 200 (APSS-200) volumetric liquid particle counter (LPC). This device is configured with a Liquilaz[®] S05 volumetric spectrometer. The Liquilaz[®] counts particles and measures their diameters by passing sample fluid through a laser beam and sensing and comparing the scattered light to diameter-dependent characteristic scattering. System software allows display of particle counts over this range in a maximum of 15 particle size bins as defined by the user. Particles counted in each bin are equal to or larger than the designated bin threshold diameter and smaller than the next larger bin threshold diameter. The result is a discrete particle size distribution over the user-defined range. The Liquilaz[®] S05 is capable of measuring diameters between 0.5 μ m and 20 μ m but counts particles with diameters up to $125 \mu m$. All particles larger than the largest defined bin diameter $(20 \mu m)$ in this study) are counted as being in the largest bin.

Sample particle size analyses using the LPC were performed on 10 mL particle samples (Table 7) diluted with an additional 10 mL of pure DI. The particle counter automatically drew three 5 mL replicates from the center of each sample. Replicate particle number concentrations (counts/mL) for each bin were averaged, adjusted for dilution, and background counts/mL subtracted. Background distributions corrected for particles present due to the DI water, sample collection vessels, and paint booth air without overspray.

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Residence Time Analysis

A residence time analysis was designed to determine the fraction of Cr^{6+} from each particle sample hypothetically available to human lung tissue at ¹ and 24 hours. Figure 11 depicts the procedural concept used to determine the fraction of Cr^{6+} dissolved from paint particles into the collection fluid after particles are allowed to reside in the fluid for ¹ or 24 hours. Samples were broken into three representative sub-samples. To determine the concentration of total Cr^{6+} collected ([Cr]_P), an untreated sub-sample with particles was digested and analyzed using atomic absorption spectroscopy. After ¹ and 24 hours, respectively, the other sub-samples were centrifuged to separate the paint particles from the sample fluid, and the fluid analyzed to determine $[Cr⁶⁺]$ resulting from Cr^{6+} dissociation from the particles ($[Cr]_{NP1}$ and $[Cr]_{NP24}$). Figure 11 shows the three subsamples originating from the particle- and Cr^{6+} -laden sample fluid. 1- and 24-hour subsamples are shown after centrifugal separation with paint particles deposited at the bottom of the centrifuge tube. Dashed lines highlight the supernatant portion of the sample, containing only dissolved Cr^{6+} ions, which was extracted for Cr^{6+} concentration analysis.

Quantifying Ci*⁺ Dissociation

This section explains the convention used to make quantitative comparisons between samples regarding Cr^{6+} dissociation. The size distribution and total amount of paint particles collected, and thus total $[Cr⁶⁺]$, varies between samples. The $[Cr⁶⁺]$ after particles were eliminated also varies depending on the total $[Cr^{6+}]$ collected and the Cr^{6+} dissociation behavior. Since comparison of dissociation behavior is central to this study, $[Cr⁶⁺]$ after particle elimination is divided by the total $[Cr⁶⁺]$ with particles and converted to a % as shown in equation 3.

$$
f_t = \frac{[Cr]_{NP}}{[Cr]_P} \times 100\%
$$
\n(3)

where: the fraction $\left(\frac{9}{6}\right)$ of Cr^{6+} dissociated at residence time t $[Cr]_P$ = the total sample Cr^{6+} concentration including collected particles $[Cr]_{NP}$ = sample supernatant (no-particle) Cr^{6+} concentration at residence time t (hours)

Henceforth, f_1 and f_2 ₄ are used when referring to the 1- and 24-hour % of Cr^{6+} dissociated in a sample or set of samples, and f_i is used when referring to both f_i and f_{24} .

Figure 11. Procedural Concept for Determining Cr⁶* Dissociation from Paint Particles (adapted from Kauth, 2001)

Sample Preservation and Preparation

Table 7 shows the total volume of collection fluid added to each sampler prior to sampling and the sub-sample volumes as divided in the laboratory after sampling. Total collection fluid volume varied according to sampler flow rate. These volumes were selected to enable the collection fluid to swirl while minimizing sample wall losses and fluid aspiration to the pumps.

1 apro μ , bampic λ bighter beneaming							
Sample or Sub-sample	Sampler Flow Rate						
	2 L/min	5 L/min	10 L/min				
Total collection fluid	30 mL	25 mL	20 mL				
Total $Cr^{\beta+}$ sample ($[Cr]_P$)	3 mL	2 mL	2 mL				
1-hr sample $([Cr]_{NP1})$	7 mL	$4-5$ mL	3 mL				
24-hr sample ([Cr]_{NP24})	7 mL	$4-5$ mL	3 mL				
Particle sample	10 mL	10 mL	10 mL				

Table 7. Sample Volume Scheduling

After each collection, samples were transferred into wide-mouth Nalgene® polypropylene containers and capped for transport to the laboratory. At the laboratory, samples were divided for analyses. 10 mL of each sample was pipetted into a glass Pyrex® beaker for particle size distribution analysis on the LPC. In order to determine the total $[Cr^{6+}]$ collected in each sampler, 2 to 3 mL of the remaining sample was pipetted into a Teflon®-lined microwave digestion vessel and an equal volume of 70% HNO₃ was added. Equal amounts of the remaining sample were then pipetted into two polypropylene centrifuge tubes. The paint particles in one centrifuge tube were allowed to remain in the DI water for ¹ hour and in the other tube for 24 hours at 37° C. This simulated ¹ and 24 hours of paint particle contact with serous lung fluid. Both samples were centrifuged after 1 or 24 hours for a minimum of 30 minutes at 4000 RPM and 37° C in order to separate the paint particles from the DI water. 2 to 3 mL of supernatant was then extracted and prepared for digestion in a similar manner to the total $[Cr⁶⁺]$ sample.

It is assumed that the supernatant $[Cr^{6+}]$ represents only the amount of Cr^{6+} dissolved from the particles after ¹ or 24 hours.

Sample Digestion

Complete decomposition of collected paint particles ensures the availability of collected Cr^{6+} for spectroscopic analysis. Microwave acid digestion was used to digest all samples. This study used an 01 Analytical microwave and employed a digestion method modified from EPA (3050A) and NIOSH (7300 and 7800) methods for paint chip digestion. Each digestion vessel was sealed and placed in the OI Analytical microwave carousel. Samples were then digested using a three to five minute temperature rise to 150°C followed by 20 minutes at 150°C. Digestion pressures ranged between 20 and 50 psig. Vessels were allowed to cool to ambient conditions and each sample was poured into a 30 mL Nalgene® High Density Polyethylene (HDPE) storage bottle. A volume of DI water equal to the sample plus $HNO₃$ volume was added to reduce $HNO₃$ concentration for analysis.

Atomic Absorption Spectroscopy (AAS)

Atomic Absorption Spectroscopy (AAS) was used to analyze the $[Cr⁶⁺]$ in each sample's total collection (with particles) and the 1- and 24-hour residence time samples (without particles). AAS sample atomization is accomplished with either a flame or electrothermal (graphite furnace) heat source. Electrothermal AAS (EAAS) is the more sensitive, though less precise, method and requires much less sample volume. EAAS is also more effective in releasing refractory metals from their matrices and is considered appropriate for samples containing less than ¹ mg/L of analyte (Willard et al., 1988). EAAS analyses were performed on a GBC Avanta Atomic Absorption Spectrometer

(AAS) configured with a PAL 3000 autosampler, graphite furnace, and deuterium background correction lamp. Selected AAS settings are summarized in Table 8. Samples with concentrations less than or equal to 4 mg/L were diluted into the EAAS calibration range and EAAS analysis performed.

EAAS calibrations were performed using a 75 μ g/L Cr⁶⁺ in 2% HNO₃ standard from High Purity Standards. A five-point calibration $(7.5, 20, 40, 60, 75 \mu g/L)$ using a concentration least-squares curve was conducted before and after every 12 samples. A minimum R^2 of .98 was required for acceptance. EAAS samples were prepared in 1 mL polyethylene cuvettes by pipetting and weighing 900 μ L of DI and 100 μ L of sample for a 0.1 dilution factor. This dilution lowered sample $Cr⁶⁺$ concentrations into the calibration range and reduced the $HNO₃$ concentration to 2-3%, making the sample matrix similar to the 75 μ g/L standard. After every 6 samples, a 75 μ g/L check sample and DI blank were analyzed as quality control measures.

System Type	Furnace
Element	Cr
Matrix	2% HNO ₃
Lamp Current	6.0 _m A
Wavelength	357.9 nm
Slit Width	0.2 mm
Slit Height	Reduced (furnace)
	Normal (flame)
Instrument Mode	Absorbance Background
	Correction Selection
Measurement Mode	Peak Area

Table 8. Summary of AAS Parameters

The AAS was programmed for a five-step EAAS graphite furnace program (Table 9). After a sample is auto- injected into the graphite furnace tube, the drying step (Step

1), heats the sample to remove all water. The drying is accomplished slowly to avoid splattering and possible loss of sample. Argon gas flows through the tube to remove evaporated vapors. Steps 2 and 3 perform sample charring and pyrolysis. These steps destroy the organic matrix components at a temperature low enough to avoid liberating the Cr. Step 4 atomizes Cr and an absorbance measurement is taken. The last step (5) cleans any residual substances from the furnace tube by raising the temperature again and forcing gas through it, preparing it for the next sample.

Re-analysis by flame AAS was conducted for all samples with Cr^{6+} concentrations greater than 4 mg/L. Flame analyses were performed on the same AAS configured with an air-acetylene burner and FS 3000 autosampler. Calibration standards were made from a 1000 mg/L Cr^{6+} standard from High Purity Standards by diluting with DI water containing 7% HNO₃. A four-point calibration curve $(1, 5, 10, 15 \text{ mg/L})$ was used for the flame method. Calibration R^2 acceptance criteria, check sample (5 mg/L) frequency, and DI blank frequency were the same as for the graphite furnace method.

Step	Final Temp $(^{\circ}C)$	Ramp Time(s)	Hold Time(s)	Gas	Read Signal
1: Drying	80	5.0	10.0	Argon	Off
2: Charring	130	30.0	10.0	Argon	Off
3: Pyrolysis	1400	15.0	15.0	Argon	Off
4: Atomization	2500	1.4	1.6	None	On
5: Clean	2700	0.5	1.5	Argon	Off

Table 9. Atomic Absorption Graphite Furnace Program

Comparing SLF to Pure De-ionized Water (DI)

Though DI does not imitate lung fluid as well as SLF, the ability to count particles in each sample was necessary for examining the role of particle size in Cr^{6+}

bioavailability. In earlier primer paint Cr^{6+} bioavailability research, SLF particle samples could not be reliably analyzed with a liquid particle counter. Instead, these studies assumed that a particle size distribution collected in a surrogate sample of DI represented the SLF particle size distribution (Kauth, 2001). This method introduces inaccuracies that limit the ability to relate a sample's particle size distribution to its Cr^{6+} dissociation. Therefore, the objectives of this study required collection of all samples in DI.

DI and SLF were tested side-by-side to verify that no significant difference exists between the fluids with regard to Cr^{6+} dissociation from paint particles. Solvent-borne epoxy primer particles were collected in DI and SLF and analyzed for Cr^{6+} dissociation. A modified version of Gamble's 1952 SLF formula (Table 10) reported by Fisher and Briant (1994) was mixed in a 1.0 L batch for use in SLF samplers. Paired t-tests were used to compare mean f_1 and f_2 for each SLF sample to a mean f_1 and f_2 for a corresponding DI sample collected simultaneously and at the same flow rate.

Description	Molecular Formula	Concentration (mg/L)		
Magnesium chloride	$MgC\frac{1}{2}$.6H ₂ O	101		
Sodium chloride	NaCl	6019		
Potassium chloride	KCl	298		
Sodium phosphate	$Na2HPO4·7H2O$	268		
Sodium sulfate	Na ₂ SO ₄	71		
Calcium chloride	CaCl ₂ ·2H ₂ O	184		
Sodium acetate	$NaH_3C_2O_2·3H_2O$	952		
Sodium bicarbonate	NaHCO ₃	97		
Sodium citrate	$Na3H5C6O7·2H2O$	97		

Table 10. Simulated Lung Fluid Ingredients

Table 11 summarizes the test results. Samples are compared by flow rate since each flow rate may collect a characteristic particle size distribution that could influence the amount of Cr^{6+} that dissociates from the primer particles. All statistical comparisons

indicate no statistically significant difference between SLF and DI values of f_1 and f_{24} . Substituting pure DI for SLF as the collection fluid does not appear to significantly alter $Cr⁶⁺$ dissociated from solvent-borne epoxy primer overspray particles.

Residence Time (hours)	Sampler Air Flow Rate (L/min)	n	% of Cr ⁶⁺ Dissociated <u>(f.)</u> SLF^*	$DI^{\#}$	Mean (paired) Differencel	statistic	t _{critical} (2-tail)*	P-value $(2-tail)$	Statistically Significant Difference?
	2	3	42% 士 81	\pm 44% 86	5%	0.524	9.925	0.652	NO.
	5	4	\pm 30% 79	\pm 33% 74	6%	0.543	5.841	0.625	NO.
	10	4	59 20% 士	18% 69 土	10%	1.31	5.841	0.280	NO.
	Aggregate Mean 11 73		12% SH.	11% 75 \mathcal{A}	3%	0.415	3.169	0.687	NO.
24	2	4	31% 84 士	97 土 9%	14%	1.19	5.841	0.319	NO
	5	4	29% 88 士	\pm 31% 71	16%	2.45	4.604	0.071	NO.
	10	4	27% 76 士	\pm 24% 88	12%	4.00	5.841	0.028	NO.
	Aggregate Mean 12 83		12% 84 SH!	± 12%	2%	0.27	3.055	0.793	NO

Table 11. SLF vs. DI Paired t-test Comparison [Solvent-Borne Epoxy Tests]

* Significance level .01

Shown with 95% confidence intervals (based on a t-distribution)

Limits of Detection and Quantitation

The typical method 3σ limits of detection (LOD), 10σ limits of quantitation (LOQ) [at 95% confidence], and sensitivities observed for both furnace and flame AAS sample analyses in this study are summarized in Table 12. LOD and LOQ represent the mean background concentration, as determined by sample blanks, plus 3σ and 10σ , respectively. Method sensitivity is defined for AAS as the concentration in μ g/mL of analyte that produces an absorbance of 0.0043 absorbance units (1.0% absorbance) [Willard, et al., 1988]. Sensitivity is shown here in μ g/L for consistency within the table.

Table 12. AAS Method Limits of Detection and Quantitation								
		Method 3 σ LOD (µg/L) 10 σ LOQ (µg/L) Sensitivity (µg/L)						
Furnace	3.7 ± 0.4	7.3 ± 0.7	$0.301 \pm .003$					
Flame	38 ± 15	$74 + 31$	65 ± 6					

Table 12. AAS Method Limits of Detection and Quantitation

Quality Control

BioSamplers were cleaned between paint particle collections to prevent buildup of paint deposits and minimize Cr^{6+} contamination from the glass samplers. The BioSampler® inlet nozzles and collection vessels were cleaned with solvents after each sample collection and then thoroughly rinsed with DI. Collection vessels were also rinsed daily using a $1:1$ HNO₃ solution followed by a DI triple rinse. Tangential nozzle stages were soaked overnight in MEK following the initial solvent cleaning, and prior to sampling they were thoroughly rinsed with DI and dried.

Despite cleaning procedures, a Cr^{6+} background, was detected throughout this study and only isolated following the final lab background collection. The tangential nozzle stages appeared to be the source of contamination, either from sample air passing over paint residue in the nozzles or Cr^{6+} leaching from the outside of the nozzles into collection fluid. Cr^{6+} Background from this source should have been reasonably consistent between sub-samples with particles ($[Cr]_P$) and those without ($[Cr]_{NP}$) since they originate from the same sample. Subtracting background decreases both [Cr]p and [Cr]_{NP} by the same amount, but the change in $\frac{[Cr]_{NP}}{[Cr]}$ depends on the % change of each [Cr]p

concentration. The larger the correction relative to either concentration, the more f_{t} decreases. For example, if the uncorrected $[Cr]_P$ and $[Cr]_{NP1}$ are 3,000 μ g/L and 2000 μ g/L, respectively, then $f = 67\%$. If both concentrations are corrected for a 200 μ g/L background, then $f_1 = 64\%$, showing that the uncorrected f_1 is a small overestimation. However, if the background is 1000 μ g/L, then $f_1 = 50\%$, a much more significant change. Background was quantified and corrected for in this study's Cr^{6+} concentration data. Correction factors specific to each sampler ranged from 200 μ g/L to 700 μ g/L. Still, unknown day-to-day inconsistencies in actual background concentration may not be represented by background correction factors. Therefore, over- or under-correcting for background possibly added variability to the data in the form of small under- or overestimations of f.

IV. Results

Primer Particle Cr⁶* Dissociation Results

Two general goals of this research were: to quantify the Cr^{6+} dissociation from primer particles into DI at residence times of ¹ and 24 hours in order to relate dissociation to residence time and particle size, and to compare the behavior of three different types of primers. Table 13 summarizes the results for all three paints with 95% confidence intervals. The mean fraction of Cr^{6+} dissociated at the indicated residence time t, (f_i), is shown for each flow rate and paint type, followed by an aggregate f for each paint over all flow rates. Tabular and graphic summaries of the background corrected concentrations of Cr^{6+} collected ([Cr]_P), 1- and 24-hour sample concentrations, and the associated f_i for all three primers are contained in Appendices A, B, and C.

Table 13. Paint Particle Cr⁶* Dissociation Summary Paint Type

<u>i unit i y</u> pu									
		Solvent-borne Epoxy $(MIL-P-23377G)^{#}$		Water-borne Epoxy (MIL-P-85582B)	Polyurethane (TT-P-2760A)				
Residence Time (hours)	Sampler Air Flow Rate (L/min)	n	Mean $%$ of $Cr6+$ Dissociated* (f_t)	n	Mean $%$ of Cr ⁶⁺ Dissociated* (f_t)	n	Mean $%$ of $Cr6+$ Dissociated* (f_t)		
	1.2	5	76 ± 23%						
	2	10	79 ± 15%	16	76 ± 7%	10	$± 4\%$ 95		
	5	16	68 \pm 10%	15	$79 \pm 8\%$	10	98 $± 2\%$		
	10	16	63 \pm 7%	15	66 \pm 7%	10	7% 91 $+$		
	Aggregate	47	70 ± 5%	46	74 ± 4%	30	94 $± 3\%$		
24	1.2	5	$90 \pm 10\%$						
	2	11	$91 \pm 8\%$	16	$82 \pm 7\%$	10	$± 3\%$ 96		
	5	16	$± 10\%$ 81	15	$± 4\%$ 90	10	- 2% 98 $+$		
	10	16	$82 \pm 7\%$	15	80 7% 土	10	4% 92 $+$		
	Aggregate	48	$85 \pm 5\%$	46	$84 \pm 4\%$	30	95 -2% \pm		

' Shown with 95% confidence intervals (based on a t-distribution)

 $#$ Includes both DI and SLF samples

In general, the solvent-borne epoxy exhibited substantial Cr^{6+} dissociation at both 1 and 24 hours. The aggregate mean f_1 was $70 \pm 5\%$ and f_{24} was $85 \pm 5\%$ suggesting that particles release the majority of their Cr^{6+} in the first hour and then release Cr^{6+} more slowly over the next 23 hours. On average, the water-borne epoxy dissociated only slightly more Cr^{6+} by 1 hour (f₁ = 74 ± 4%) than the solvent-borne epoxy and essentially the same amount by 24 hours ($f_{24} = 84 \pm 4\%$). On the other hand, data indicate that the polyurethane primer consistently released almost all of its Cr^{6+} by 1 hour (f_i = 94 \pm 3%) and $f_{24} = 95 \pm 2\%$). This primer demonstrated strong hydrophobic characteristics, which caused a portion of the paint particles to separate from the DI water and visibly "cling" to the sides of the collection vessel producing a paint film. Collection vessel wall losses could exaggerate Cr^{6+} dissociation estimates. If primer on the vessel wall leached Cr^{6+} into the fluid but retained Cr^{6+} that was not accounted for in the total $[Cr^{6+}]$ with particles estimate, $[Cr]_P$, then f for the polyurethane would be an overestimation of the dissociation from particles residing in the fluid.

Primer Volatiles Testing

It was theorized that Cr^{6+} dissociation into fluid from primer overspray particles might be limited to that from unevaporated solvents (volatiles) containing dissolved chromate. Based on this hypothesis, a significant increase in the water-borne f was expected due to an increase in: the solubility of $SrCrO₄$ in the water-borne primer's volatile fraction (which includes water), the solubility of the mainly-water volatiles in lung fluid, or the fraction of volatiles in the paint mixture. As discussed earlier, solventborne primer volatiles consist of solvents while water-borne primer volatiles include both water and solvents. The water-borne epoxy volatiles represent 74% of that primer by

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volume and water makes up 77% (by volume) of the volatiles. By contrast, both solventborne primers contain only 41% volatiles by volume.

Quantitative tests were conducted to assess the $[Cr⁶⁺]$ in each primer's volatile fraction after paint mixing and equilibration. Three 10 mL samples of each paint were centrifuged for 20 minutes at 4000 RPM in order to separate the less dense volatiles in each paint. A sample of the solvent- or solvent-and-water-comprised supernatant was then extracted, microwave-digested using $HNO₃$, and analyzed using furnace and flame AAS. The solvent-borne epoxy volatiles had a mean $[Cr^{6+}]$ of 586 ± 181 μ g/L (n = 3) and the water-borne epoxy volatiles a mean of $374,000 \pm 90,000 \,\mu g/L$ (n = 3) [95% confidence], a more than 600 fold increase in dissolved Cr^{6+} . Based on the SrCrO₄ solubilities given in Chapter 2 (45,000 μ g/L in MEK and 1,200,000 μ g/L in water) neither primer volatile sample was near $SrCrO₄$ saturation. Further calculations show that the observed $[Cr^{6+}]$ in the solvent- and water-borne volatiles represents only .0009% and 1.3% of the total mass of Cr^{6+} per volume of paint, respectively. This means that most of the $SrCrO₄$ in the mixed paint is in solid particle form and a very small fraction is dissolved in the volatiles when the primer is sprayed.

The polyurethane volatile fraction mean $[Cr^{6+}]$ was 492,000 \pm 139,000 μ g/L (n = 3). This far exceeds the expected $SrCrO₄$ saturation limit but is still only 1.4% of the total Cr^{6+} mass per volume of paint. Unfortunately, the validity of this primer's samples is questionable due to difficulty separating and sampling a "pure" solvent supernatant. As a result, polyurethane volatile samples may have contained non-volatile paint constituents including un-dissolved $SrCrO₄$ pigment.

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Primer Type Comparison

Quantitative comparison of mean £ by paint type, residence time, and sampler flow rate indicates some minor differences in dissociation behavior. Using JMP 4.0, an analysis of variance (ANOVA) and a Tukey-Kramer all pairs analysis were performed. The Tukey-Kramer analysis is a simultaneous multiple comparison of the means and was performed at an overall significance level of α = .05. Figure 12 shows the results of each comparison with underlines connecting data sets that indicate no statistically significant difference in f_t . In no case do the solvent- and water-borne epoxies show a significant difference in their mean f.

	$t = 1$ hour	
2 L/min $(R^2 = .24)$ <u>Water-epoxy</u>	Solvent-epoxy	Polyurethane
<u>5 L/min (R^2 = .34)</u> Solvent-epoxy	<u>Water-epoxy</u>	Polyurethane
<u>10 L/min (R^2 = .48)</u> Solvent-epoxy	Water-epoxy	Polyurethane
<u>Aggregate (R^2 = .35)</u> Solvent-epoxy	Water-epoxy	Polyurethane
	$t = 24$ hours	
<u>2 L/min ($R^2 = .20$)</u> <u>Water-epoxy</u>	Solvent-epoxy	Polyurethane
<u>5 L/min (R^2 = .21)</u> Solvent-epoxy	Water-epoxy	Polyurethane
10 L/min $(R^2 = .16)$ $Water\text{-}epoxy$	Solvent-epoxy	Polyurethane
Aggregate $(R^2 = .13)$ Solvent-epoxy	Water-epoxy	Polyurethane

Figure 12. Tukey-Kramer All Pairs Analysis by Flow Rate and Residence Time

Though ANOVA and the Tukey-Kramer comparison do indicate a difference in the polyurethane f_i , high variability in the solvent- and water-borne data limits the amount of overall variance that can be attributed to the difference in primers (note the small values of \mathbb{R}^2). Figure 13 compares the data using a box and whiskers plot of each primer's aggregate f_1 and f_2 data. The "whiskers" at the top and bottom of each plot denote the highest and lowest values. Long horizontal lines represent the mean f_t , short lines within each box are at the median, and the lower and upper end of each box depict the $25th$ and $75th$ percentiles, respectively. Data points outside the "whiskers" represent outliers, defined as values > 1.5 times the fourth spread (i.e. $75th$ percentile $-25th$) percentile) from closest end of the box (Devore, 2000). Ultimately, the data suggest no evidence for a difference in Cr^{6+} dissociation from the solvent- and water-borne primers, but do point toward a different behavior for the polyurethane.

Figure 13. Box and Whiskers Comparison $(f_1 \& f_2)$ by primer type)

Residence Time Comparison

The results indicate that the majority of Cr^{6+} dissociation takes place in the first hour after which there is generally some further dissociation through at least 24 hours. An indication of this behavior is the relatively small mean differences $(f_{24} - f_1)$ for paired samples, and the associated mean percent increase in f_i (Table 14). The mean percent increase is defined here as the amount of change relative to f_1 , or $[(f_{24} - f_1)/f_1] \times 100\%$. Table 14 also shows paired t-test results comparing mean f_1 and f_2 4 for each paint and flow-rate combination. Despite the appearance of little change, the t-tests indicate that a statistically significant increase in the fraction of Cr^{6+} dissociated from the solvent- and water-borne epoxy primer particles does occur. The polyurethane primer's lack of significant additional dissociation after ¹ hour is, at least partly, due to its near complete dissociation at ¹ hour.

Primer	Sampler Air Flow Rate (L/min)	n	1-hr Mean $%$ of Cr^{6+} Dissociated ¹ (f_1)	24-hr Mean $%$ of Cr^{6+} Dissociated ¹ (f_{24})	Mean (paired) Diff. $(f_{24} - f_1)$	Mean %	Increasel statistic	^T critical $(right-tail)^2$	P-value $(1-tail)$	Statistically Significant Increase χ^2
Solvent Epoxy	1.2	5	76%	90%	14%	18%	2.48	2.132	0.034	YES
(MIL-P-23377G)	2	10	79%	91%	12%	15%	2.03	1.833	0.037	YES
	5	16	68%	81%	12%	18%	3.95	1.753	0.001	YES
	10	16	63%	82%	19%	29%	5.45	1.753	< 0.001	YES
	Aggregate	47	70%	84%	15%	21%	7.01	1.68	< 0.0001	YES
Water Epoxy	2	16	76%	82%	7%	9%	3.17	1.753	0.003	YES
(MIL-P-85582B)	5	15	79%	90%	11%	14%	3.48	1.761	0.002	YES
	10	15	66%	80%	13%	20%	7.14	1.761	< 0.001	YES
	Aggregate	46	74%	84%	10%	14%	7.14	1.681	< 0.001	YES
Polyurethane	2	10	95%	96%	1%	1%	0.657	1.833	0.264	NO.
(TT-P-2760)	5	10	98%	98%	0%	0%	<< .0001	1.833	0.500	NΟ
	10	10	91%	92%	1%	2%	0.756	1.833	0.234	NO
	Aggregate	30	94%	95%	1%	1%	0.897	1.699	0.377	NO

Table 14. Residence Time Comparison (Paired t-tests)

Means for *paired* samples only

? Significance level .05

 3 Includes both DI and SLF samples

Primer Particle Distributions

Figures 14, 15, and 16 display the background corrected particle size distributions, averaged by sampler flow rate, collected in this study. Generally, increasing sampler air flow rates produced the desired increase in the number of larger particles, as seen by the rightward shift with flow rate. All collected distributions are shown graphically in Appendices A, B, and C by paint and flow rate. The LPC counts particles per bin per mL of sample. Though these counts are in discrete bins, they are depicted as continuous distributions for ease of comparison. The midpoint d_p of each bin is used to represent the particle sizes collected. Since the LPC counts particles ≥ 20 and $<$ 125 μ m in the 20 μ m bin, particles in the 20 μ m bin were extrapolated out to smooth the distributions for display and later calculations. Extrapolation methods are described in Appendix D.

Figure 14. Solvent-borne Epoxy Average Particle Size Distributions by Flow Rate

Figure 15. Water-borne Epoxy Average Particle Size Distributions by Flow Rate

Figure 16. Polyurethane Average Particle Size Distributions by Flow Rate

In general, the 1.2 and 2 L/min samplers collected small particles very efficiently but very few particles larger than $5 \mu m$. On the other hand, the typical 10 L/min distribution had very few particles $\leq 2 \mu$ m and contained particles in all bins, including \geq 20μ m. Six of the 10 L/min water-borne epoxy samples showed a notably different

distribution, containing only particles larger than 3.5μ m (Appendix B-2) and significant numbers of particles in all bins up through 20 μ m. These six distributions all occurred in high flow rate samples collected in the same three sampling sessions, and had similar numbers of total particles and $[Cr]_P$ to other samples, but cannot be explained. Finally, note that the polyurethane samples show a substantial decrease in the quantity of particles collected, and a distinctly different set of average distributions. The tendency of polyurethane particles to "cling" to collection vessel walls may explain why fewer particles were collected during spray times comparable in duration to those of the other paints.

Calculating Aerodynamic Diameters and the Cr ⁺ Distribution

Two conversions were necessary to interpret the collected particle distributions in terms pertinent to lung physiology and Cr^{6+} bioavailability. First, since inhaled particles distribute in the lung based on aerodynamic diameter (d_{ae}) , each particle size bin (midpoint) d_p was converted to an equivalent d_{ae} . Particle density directly influences d_{ae} , such that the more particle density exceeds 1 $g/cm³$ the more its d_{ae} exceeds its d_p (see Ch. 2). Due to the high density of Cr relative to the other paint constituents, Cr^{6+} (as SrCrO₄) is largely responsible for the difference between d_p and d_{ae} for chromatecontaining primer particles. The increase in $\%$ mass of Cr^{6+} with particle size causes paint particle density (ρ_p) to increase as d_p increases (see Figure 5) [LaPuma et al., 2001; Novy, 2001; Rhodes, 2002]. Therefore, conversions of d_p to d_{ae} are unique to each d_p , and also to each paint since the Cr^{6+} bias differs between paints. The second conversion involved determining the volume of Cr^{6+} collected at each particle size by incorporating the Cr^{6+} bias into collected particle volume distributions. Conversion of each bin d_p to d_{ae} and calculation of the % volume of Cr^{6+} in particles of each bin d_p was needed to determine the Cr^{6+} volume distribution as a function of d_{ac} .

A summary of data obtained from MSDSs and Deft® Product Information Data Sheets is given in Table 15. The calculated % mass of Cr^{6+} in the "wet" paint mixture for each primer is included with this data. Paint mixture composition data from Table 3 was used to determine the density of the non-SrCrO₄ fraction of each primer and the $\%$ volume of $SrCrO₄$ in the paint mixture. Table 16 shows the $Cr⁶⁺$ bias data from the Novy (2001) and Rhodes (2002) studies as a mass % (mass of Cr^{6+} to mass of dry paint) for each bin, defined by a lower-limiting effective cutoff diameter (ECD).

Table 15. Calculation Data (MSDS and Deft® Product Information Data Sheets)

Primer Type	Mixed paint density (ρ_{wet}) [g/L]	% Volume of solids $(\mathbf{v}_{\rm solids})$	Solids density $(\rho_{\rm dry})$ [g/L]	Paint mixture $\%$ mass Cr^{6+}
Solvent-epoxy	1240.2	58.55%	1539.8	5.19%
Water-epoxy	1102.3	26.39%	1447.5	2.58%
Polyurethane	1173.1	59.63%	1393.6	3.03%

Note: Data represents the paint mixture as sprayed and units have been converted from English to SI

	Mean % Cr^{6+} (mass $Cr^{6+}/$ mass dry paint)				
Particle Size	Solvent-epoxy ¹	Water-Epoxy	Polyurethane ²		
(ECD) [µm]	(Deft® 02-Y-40)	(Deft® 44-GN-72)	(Deft _® $09-Y-2$)		
0.7	$0.8\,\%$	0.67%	0.36%		
1.0	1.2%	0.72%	0.51%		
1.6	1.8%	1.15%	0.90%		
2.6	2.5%	2.89%	1.65%		
2.7	2.9%	1.89%	1.70%		
4.1	4.5%	4.95%	2.51%		
4.3	3.9%	4.97%	2.79%		
6.2	5.8%	6.50%	3.77%		
7.0	4.6%	6.56%	3.72%		
9.5	5.3 %	6.67%	3.86%		
11.4	6.2%	N/A	N/A		
14.5	5.8%	6.27%	3.76%		
22.2	5.7 $%$	5.57%	3.60%		
34.1	5.3%	6.03%	4.34%		

Table 16. Cr6+ Content Bias Data (Novy¹ , 2001; Rhodes² , 2002)

Appendix E describes in detail the calculations necessary to determine ρ_p , d_{ae} , and the Cr^{6+} volume fraction for each d_p collected. The calculations make several key assumptions:

- 1) Collected paint particles are spherical
- 2) Cr^{6+} in the paint droplets is in the form of SrCrO₄
- 3) Collected paint particles comprise a mixture that is homogeneous with respect to all constituents except $SrCrO₄$, and is otherwise representative of the batch paint mixture
- 4) Dry paint contains only paint solids such that the solids density may be used to approximate the dry paint density
- 5) Linear interpolation of dry paint particle $Cr⁶⁺$ content data may be used to approximate the % mass of Cr^{6+} in each particle size

Figure 17 depicts the conceptual model for calculating the density (ρ_p) and Cr^{6+} volume fraction (v_{Cr}) of a particular size particle. Though ECD is a function of particle aerodynamic diameter, it is assumed to be a valid first approximation of d_n . Based on this assumption, each computation started by interpolating the mass fraction $\frac{6}{6}$ of Cr⁶⁺ in a *dry* paint particle of each bin midpoint d_p (hereafter denoted as the bold d_p) from Table 16 (Step 1). The $drv Cr^{6+}$ mass fraction was then converted to the mass fraction $(\%)$ of $SrCrO₄$ in a *wet* particle of size d_{p} (Step 2) by first "returning" the volatiles to the particle and adjusting the Cr^{6+} mass fraction for the accompanying increase in particle volume. In step 3, the SrCrO₄ mass fraction is converted to the volume fraction $(\%)$ of SrCrO₄ in a *wet* particle of size d_p . Using the volume fraction of $SrCrO_4$ and that of the other paint constituents the density specific to each d_p , denoted as the bold ρ_p , was computed using the known densities of SrCrO₄ and non-SrCrO₄ constituents. Each ρ_p was then used to determine a d_{ae} and Cr⁶⁺ volume fraction (v_{Cr}) for each d_p . The v_{Cr} values were applied as a correction factor to the total particle volume per mL of sample collected in each bin to account for the difference in Cr^{6+} content with particle size. The result is a Cr^{6+}

volume distribution (μ m³ Cr⁶⁺/mL sample) for each sample (Figures 18, 19, and 20). Computed v_{Cr} values for each bin are shown in the data summary tables of Appendices A, B,and C.

Figure 17. Determining Size-Specific Particle Density and Ci*"⁺ % Volume

 Cr^{6+} volume distributions demonstrate that a majority of the Cr^{6+} volume resides in particles with aerodynamic diameter larger than those that deposit in the pulmonary or tracheobronchial regions (reference Figure 3), despite collecting many more smaller particles than larger ones. More importantly, for this study, the Cr^{6+} distributions have been corrected for the bias in Cr^{6+} , which adjusts for the fact that different particle sizes contain unequal fractions of Cr^{6+} .

Figure 18. Solvent-borne Epoxy Cr⁶⁺ Volume Distributions Collected

Figure 19. Water-borne Epoxy Cr^{6+} Volume Distributions Collected

Figure 20. Polyurethane Cr⁶* Volume Distributions Collected

Relating Particle Size to Cr⁶* Dissociation Behavior

An important objective in this study was to assess the relative contributions of various particle sizes to Cr^{6+} dissociation from primer particles. One hypothesis was that smaller overspray particles release Cr^{6+} more readily than larger particles. If this is true there should be a positive correlation between the samples with many small particles and the fraction of Cr^{6+} that dissociates from the particles (f_i). It follows that samples with a greater proportion of large particles would have a relatively smaller f. Correlations comparing the volume of Cr^{6+} collected in each particle size bin to sample f_i were used to see if data indicate the existence of particle size-dependent Cr^{6+} dissociation.

Prior to statistical analyses, data conversion was necessary to obtain accurate and unbiased parameters for comparison. First, particle number concentrations (N_i) in particles/mL for each bin (i) of each sample were converted to a volume of Cr^{6+} per mL

of sample for each bin (V_{Cri}) using equation 4, such that:

$$
\frac{\text{Cr Volume/mL}}{\text{Bin}} = \frac{\# \text{of particles/ mL}}{\text{Bin}} \times \frac{\text{Particle Volume}}{\text{particle}} \times \frac{\text{Cr Volume}}{\text{Particle Volume}}.
$$
\n
$$
V_{Cr_i} = N_i \cdot \left(p \cdot \frac{d_i^3}{6} \right) V_{Cr_i}
$$
\nwhere:
\n
$$
V_{Cr_i} = \text{volume of Cr}^{6+} \text{per mL sample in bin i}
$$
\n
$$
N_i = \text{particle number concentration in bin i (particles/mL)}
$$
\n
$$
p \cdot \frac{d_i^3}{6} = \text{the volume of a spherical particle with bin i mean diameter, d_i}
$$
\n
$$
V_{Cr_i} = (Vol. of Cr)/(Vol. of wet paint) \text{ in a particle mean bin diameter d_i}
$$
\n[corrects for Cr⁶⁺ bias]

i $=$ the bin number ranging from $i = 1$ for the 0.5 μ m bin to $i = 15$ for the $\geq 20 \mu m$ bin

Next, the volume of Cr^{6+} per mL in each bin was divided by the total volume of $Cr⁶⁺$ per mL collected in the same sample (V Cr_{total}) as in equation 5. The result is an estimate of the fraction of collected Cr^{6+} residing in each particle size bin (i) for each sample, denoted as Fc_{ri}. By normalizing the Cr^{6+} volume in each bin to the total Cr^{6+} volume, F_{Cri} is adjusted for both the bias in Cr^{6+} content (using V_{Cr}) and in particle

volume (V =
$$
\frac{p \cdot d_i^3}{6}
$$
). This adjustment corrects for the fact that different particle sizes

have inherently different volumes and % Cr^{6+} and, therefore, unequal supplies of Cr^{6+} to contribute to the collection fluid through dissociation. As a result of these corrections Fc_{i} is an unbiased parameter, and is appropriate for correlations to f_i .

$$
F_{Cr_i} = \frac{(Cr \text{ Volume/mL}) \text{ /Bin}}{\text{Total Cr Volume/mL}} = \frac{V_{Cr_i}}{V_{Cr_{total}}} = \frac{\left[N_i \cdot \left(p \cdot \frac{d_i^3}{6}\right) \cdot V_{Cr_i}\right]}{\sum_{i=1}^{15} \left[N_i \cdot \left(p \cdot \frac{d_i^3}{6}\right) \cdot V_{Cr_i}\right]}
$$
(5)

To gain information about the relationship between the amount of Cr^{6+} collected in particular particle sizes or size ranges and Cr^{6+} dissociation, each Fc_{ri} was statistically correlated with its accompanying sample f_1 , f_2 ₄, and the change ($\Delta f_1 = f_2$ ₄ - f_1). The underlying relationship between the fraction of the total $Cr⁶⁺$ that dissociates from collected particles (f) and the distribution of that Cr^{6+} with particle size (Fc_{r1}, Fc_{r₂,... Fc_{r₂₃)}} is depicted by equation 6.

$$
f_{t} = \sum_{i=1}^{15} F_{Cr_{i}} \cdot F_{t,i}
$$
 (6)

where: F_{ti} $=$ the probability that, or frequency with which, the fraction of Cr^{6+} resident in bin i (Fc_i) dissociates by time t

In other words, within each sample, particles of every size release some portion $(F_{t,i})$ of their Cr^{6+} to the DI (0 to 100%), and in so doing contribute to the fraction of total Cr^{6+} dissociation, f. Hence, equation 6 may be thought of as defining a theoretical expected value (mean) for the fraction of Cr^{6+} that dissociates from a given particle sample (f). In this analogy the fraction of Cr^{6+} resident in each bin (F cr_i) is a discrete random variable and $F_{t,i}$ is a hypothetical probability mass function.

Spearman Correlations

Figures 21, 22, and 23 depict the results of a correlation analysis for the three primers. The $0.5 \mu m$ bin (bin 1) correlations are not shown for the solvent- and waterborne epoxies as particle counts in these bins were below background in all but two (solvent epoxy) samples. This bin is subject to substantial interference from non-paint particles. The distribution of Fc_i for a single particle size bin over all samples was not normally distributed for bin sizes less than $14 \mu m$ and greater than $20 \mu m$, therefore the non-parametric Spearman Correlation Coefficient (ρ) was used as the test statistic. This coefficient is a distribution- free estimate of the degree of linearity between two variables and has a range of +1 (positive relationship) to -1 (inverse relationship). Spearman ρ coefficients are depicted in graphic and tabular form for pairs of correlated variables, and P values are shown as an indication of the statistical significance of those coefficients. d_p for each bin (i) is also included as a reference.

Figure 21. Solvent-borne Epoxy Spearman Correlations Shaded bars indicate correlations with P-values < .100.

Figure 22. Water-borne Epoxy Spearman Correlations

Shaded bars indicate correlations with P-values < .100.

Figure 23. Polyurethane Spearman Correlations Shaded bars indicate correlations with P-values < .100.

All three primers show some significant correlations. The solvent- and waterborne epoxy primer data demonstrate generally higher significance than the polyurethane, as indicated by the P-values. Shaded bars in Figures 21, 22, and 23 highlight correlations with P-values ≤ 0.1 . Correlation coefficients for both epoxy primers show a positive correlation for the smallest particle sizes and a negative correlation for larger particles. Though this pattern is significant for the solvent epoxy f_1 correlations, the f_2 correlations are much weaker and none show statistical significance. To the contrary, the water epoxy results show a similar pattern at both ¹ *and* 24 hours with even stronger correlation and high statistical significance. The water epoxy also shows a feature that cannot be explained. The largest particles ($d_p \ge 20 \,\mu$ m) demonstrate a positive correlation with f_t that is similar in magnitude and significance to the smallest particles (1.5 μ m $\le d_p \le 4.3$) μ m). Finally, the polyurethane data only show a significant correlation (positive) at 1 and 24 hours for the smallest particle bin ($d_p = 0.75 \,\mu \text{m}$), though its overall trend is similar to the epoxy primers. Given that the polyurethane showed very little variability in f_t , the lack of significant correlation between f_t and Fc_{t_i} for that primer is understandable. The observed patterns indicate that the amount of $Cr⁶⁺$ contained in smaller primer particles has a stronger influence on how much Cr^{6+} is released to the collection fluid during the first 24 hours than does Cr^{6+} residing in larger particles.

Correlations of Fc_i with Δf_i , particularly for the solvent epoxy, add further insight into the data. The solvent epoxy shows a significant negative relationship ($\rho = -0.51$ to -0.31) between Fc_{ri} and Δf_t for particles $\leq 2.8 \mu$ m and a positive relationship ($\rho = +0.46$) to $+0.11$) for all particles larger than 4.3 μ m. A similar pattern was observed in the water

epoxy primer, but correlations are weaker and less significant. The polyurethane data show a positive correlation between Fc_{ri} and Δf_t over the range 4.3 μ m to 11.8 μ m, though statistical significance is somewhat limited. The pattern seen in the Δf_t correlations, when combined with those for f_1 and f_2 , supports the theory that very small particles release their Cr^{6+} rapidly (the observed positive correlation to f_i) but contribute little to the dissociation between ¹ and 24 hours (the observed negative correlation with Δf_t). Furthermore, the indication is that large particles are slower to release their Cr^{6+} (the observed negative correlation to f_i) but do provide a residual source of dissolvable Cr^{6+} over the first 24 hours in DI (the observed positive correlation with Δf_t). This implies that distributions with greater numbers of small particles release a larger proportion of Cr^{6+} and do so quickly.

V. Discussion

Summary and Conclusions

The objectives of this study were to examine three aspects of Cr^{6+} dissociation from chromate-containing primer particles into a fluid:

- 1) The influence of particle residence time in pure DI (water) on the quantity of Cr^{6+} dissociated
- 2) Differences in Cr^{6+} dissociation between three different primer compositions (solvent-borne epoxy, water-borne epoxy, and solvent-borne polyurethane)
- 3) The relationship between particle size and Cr^{6+} dissociation

These objectives have direct implications for bioavailability, and ultimately the toxicological impact, of Cr^{6+} inhaled in this form. Time-dependent dissociation (objective 1) is important due to the body's ability to escalate and remove Cr^{6+} containing particles from the lung. It follows that understanding any size-dependent dissociation (objective 3) is important because the location of particle deposition in the lung, and thus the time required to escalate and clear those particles, depends on particle (aerodynamic) diameter. Finally, it was proposed that encapsulation of Cr^{6+} in a paint matrix may render it less available in lung fluid after some initial release of Cr^{6+} , and that this effect may vary depending on paint composition (objective 2).

The data suggest that, for the three aircraft primers tested, a substantial release of $Cr⁶⁺$ into DI from overspray particles does occur during the first hour of contact with the DI. The solvent-borne epoxy primer did not show the apparent Cr^{6+} -binding observed in earlier research and, was not significantly different from the water-borne epoxy. Between ¹ and 24 hours of particle residence time, the solvent- *and* water-borne primers show a statistically significant increase in the fraction of Cr^{6+} dissociated, though the additional fraction dissociated is relatively small. During the first hour in DI, solvent

epoxy particles dissociate Cr⁶⁺ at a rate of 70 \pm 5% and the water epoxy 74 \pm 4%, but only dissociate an additional 15% and 10%, respectively, by 24 hours. Testing of the $[Cr⁶⁺]$ in each primer's mixed volatile fraction confirmed that almost 100% of the SrCrO₄ in these primers remains in solid, undissolved, form in these primers. Therefore, the f_i data indicate that paint constituents other than the volatiles, including solid $SrCrO₄$, must be sources of Cr^{6+} to the DI. Consequently, the hypothesis that the water-borne epoxy releases significantly more Cr^{6+} into a watery fluid than the solvent-borne epoxy is not supported.

The polyurethane primer demonstrated a distinctly different pattern, releasing essentially all of its Cr^{6+} within the first hour (94 \pm 2%). However, some doubt is cast on this paint type based on the observation that it tended to "cling" to collection vessel walls. This observation inspired a separate qualitative test. Small volumes (< 10 mL) of mixed polyurethane primer were poured directly into a 1.0 L beaker of DI and swirled. The paint appeared to immediately separate some of its components, possibly the solvents separating from the pigment and resin solids. Swirling moved the majority of the solids to the walls of the vessel where they formed a hydrophobic film. These observations coincide with the clear appearance of the polyurethane samples and the film observed on collection vessel walls. It may be that polyurethane particles released some amount of $Cr⁶⁺$ dissolved in the more water-soluble constituents upon contact with the DI, but separated the bulk of the $SrCrO₄$ (the source) from the fluid to the vessel walls. Loss of $Cr⁶⁺$ -containing paint constituents to collection vessel walls would result in systematic overestimation of f due to underestimating the total amount of Cr^{6+} ($[Cr]_P$) that had the opportunity to release Cr^{6+} .

Although study data indicate a large fraction of Cr^{6+} dissociates from chromatecontaining primer particles, calculations show that most of the Cr^{6+} mass collected was in the larger overspray particles. This implies that despite the large number of small particles $(d_p < 5 \mu \text{m or } d_{ae} < \approx 6 \mu \text{m})$ in primer overspray, most of the Cr⁶⁺ volume exists in larger particles that are less likely to be inhaled or are quickly cleared from the upper respiratory system upon deposition. Correlations indicate that Cr^{6+} contained in smaller overspray particles dissociates more quickly and more completely than the Cr^{6+} in larger particles. Observed sample f_1 and f_2 ranged from complete (100%) dissociation to as low as $f_1 = 32\%$ and $f_2 = 33\%$ for the solvent epoxy, and $f_1 = 44\%$ and $f_2 = 48\%$ for the water epoxy. This range of f_i appears to result from a dependency on sample particle size distribution. The significance of such a dependency is that Cr^{6+} may be released more slowly from larger particles that deposit higher in the respiratory system.

Several factors, when considered together, point toward a difference in the character of Cr^{6+} exposure from chromate-containing primer overspray as compared to other industrial exposures to chromate-containing particles. These are: the tendency of Cr^{6+} to remain predominantly in an undissolved (solid SrCrO₄) form in primer paint, the small Cr^{6+} mass in respirable overspray particles, and the degree of Cr^{6+} dissociation from deposited paint particles. Limited Cr^{6+} dissociation from larger particles, containing the preponderance of Cr^{6+} , may be the reason for the lack of significant lung cancer incidence among painters relative to other chromate-exposed workers. If painters inhale only a small amount of overspray that contains only the smallest, $d_{ae} < 6 \mu m$, particles possessing very little Cr^{6+} then exposure may be limited, even if ventilation and respirator protection fail or are improperly used.

Study Limitations

Limitations exist in this study. As mentioned, daily variations in $[\text{Cr}^{6+}]$ background could not be quantified and may have introduced bias even after a mean correction was applied. Second, values of f_f may be exaggerated if a portion of collected primer particles were in contact with the fluid long enough to leach Cr^{6+} into the DI, but were lost prior to [Cr]p analysis. As mentioned earlier, this may have occurred as a result of particle adhesion to collection vessel walls, which was especially noticeable for the Polyurethane primer.

Recommendations

This study points to several possible ways to improve future research regarding $Cr⁶⁺$ bioavailability from primer paints, and generates new questions for further study. Future studies using BioSamplers to collect primer paint particles must control contamination. In addition to rinsing the collection vessels with $1:1 \text{ HNO}_3$, the tangential nozzle stages should be soaked in $1:1 \text{ HNO}_3$ followed by ultrasonic cleaning to remove paint residue. A second $1:1$ HNO₃ rinse should then be performed to eliminate adsorbed Cr from the glass nozzle stages prior to DI rinse. Second, any future study concerning the bioavailability of $Cr⁶⁺$ from primer paint particles or other similar chemical matrices should include a chemical analysis of the matrix. Better understanding about Cr^{6+} solubility in the various paint constituents, the solvent polarities, and mechanisms for $Cr⁶⁺$ transfer would provide useful insight into the questions posed in this study. For example, a surface mass transfer model with some matrix limiting may explain the dissociation behavior seen in this study. Microscopic analyses may add further understanding as to overspray particle behavior in fluid, to include particle shape,

composition, whether or not particle agglomeration occurs, etc. Finally, using a lung mucous layer surrogate as the particle collection medium would more closely represent particle deposition and subsequent Cr^{6+} dissociation in the mucous layer. Although particle size analysis may be more difficult for collections in mucous, primer particle or chromate solubility in the mucous may differ from that in water or SLF.

Modifications to methodology are necessary to develop a firmer quantitative estimate of the apparently size-dependent Cr^{6+} dissociation behavior observed in this study. Determining the Cr^{6+} dissociation (0 to 100%) from different size particles is possible by solving equation 7 for $F_{t,i}$. An accurate solution requires samples that contain single particle diameters (or as close to this as possible), so as to reduce or eliminate multiple dependencies within samples. The particle size distributions collected in this study, though somewhat variable, were not distinct enough to allow consistently meaningful solutions even when particle sizes were grouped to reduce the number of variables. The inherently high concentration of small particles in overspray makes the technique of varying sampler flow rate within feasible limits inadequate for collecting distinctly different distributions. Though ultrasonic nebulizer technology may enable mono-disperse overspray particle size distributions to be generated and collected, it may not be representative of spray gun atomization. Instead, it may be desirable to focus on changing collection methodology.

Combining a particle separation technology, such as cascade impaction or electrostatic precipitation, with impinger-type collection may allow different particle sizes to be selectively collected into fluid by using the separation apparatus as a bandpass filter. Then, applying the concepts developed in this study, direct quantitative

determination and, therefore, prediction of the mass of $Cr⁶⁺$ released as a function of particle size becomes possible. This capability may have tremendous value to bioavailability studies concerning inhalation of particles containing toxic compounds in a complex matrix.

Glossary

The following list defines terms and symbols used in the text and Appendices:

Appendix A:

Deft_® 02-Y-40 Solvent-borne Epoxy Polyamide Primer (MIL-P-23377G)

Appendix A-1: Solvent-borne Epoxy Data Summary

 $=$ Flame AAS results

Appendix A-2: Solvent-borne Epoxy Particle Size Distributions by Flow Rate

.6+1 Appendix A-3: Solvent-borne Epoxy Particle Sample DI [Cr] vs. Time

The chart above depicts the Cr^{6+} concentration data from the data summary table (Appendix A-1). Lines connect [Cr]P, the concentration of total Cr^{6+} collected (including that in particles) in each sample, to that sample's 1-hour ([Cr]NPl) and 24-hour ($[Cr]NP24$) concentration from dissociated $Cr⁶⁺$ (i.e. with particles removed).

Appendix A-4a: Deft_® Solvent-borne Epoxy Primer (Base) MSDS Excerpt

 \mathbf{g}_{in} $^\mathrm{4}$ $_\mathrm{Page}$: 1 MATERIAL SAFETY DATA SHEET Printed $\approx 07/19/01$ For Coatings, Rezins and Related Noterials .
In them to be about the code of the company of the co SECTION I - PROBUCT INDENTIFICATION Manufacturer: DEPT, INC. (CAGE CODE 33461) - Information Phone: (949) 474-0400
- Nanufacturer: DEPT, INC. (CAGE CODE 33461) - Information Phone: (949) 474-0400
- INGLINE - CHENTREC - Phone: 000-424-9300
- IRGINE - CA IRVINE $-CA$ 92014 C.A.S. Number WWW 199-41-4 - 9 1 109 ppm 125 ppm 108 ppm
- TARC has determined that ethylhemsene is possibly sactras determines that ethylogicans is possibly

excelnogenic to Bunnes.

872-50-4 × 1. N.K. N.K. N.K.

N-HETNATHROLLINGER CAS N.W. 2004, ESTIMATED TAM TWA

N-HETNATHROLLINGE COLORATION: 1905-000 % NETHLETRAOLICOME $M.E = 15.6.77F$ HO FEM. (FER GAF CORPORATION) THE ABOVE LISTED PRODUCTS ARE ON THE TECA INVENTORY LIST ALSO ANY UNLISTED INGREDIENTS. N.E. : Not Established $\begin{tabular}{c|c|c|c|c|c|c} \hline & \multicolumn{3}{c}{SPC1100} & \multicolumn{3}{c}{$ sway, Rate: $f_1 \pm 6$ & $r = 100(y)$, Regard assumpts when are very simple than Mater.
Weblatiies you & 44.8 Ways 21.6 Web initiate control in the Weblatiies you & 44.8 Ways 21.6 Web per gallon. IL21 Pounds.
Appearance: YEL AUVOLCALITION TENPERATURE: No information found
DECONFOSITION TENPERATURE: No information found CORROSICA RATE: No information found with common
VISCOSTT: This liquid to beavy viscude material SECTION IV THE AND EXPLOSION NATARR BATA
Flamability Class: IB Flash Toint:46 F TCC LEL: 0.994 UEL: 18.508
-EXT(HOMESHIRE MEDIA: 0.994 UEL: 18.508
-CATALOGISTIC PORT CHARLAL, WHTER FOOT"
-CONNAL ALCOHOL: 2000 FORM, ALCOHOL FORM, CO2. DRY CHERICAL, WATER FOG**
-SPECIAL FIREFIGNITHOR FRONTEDURES:
-SPECIAL FIREFIGNITHOR FRONTEDURES:
FORM ALCOHOL FORM problems and the article of the containers to prevent
injuring apparation and the ma a
A server ver er var en en verske provinser var en verske var en verske var en v -PERMISSIBLE EXPOSURE LEVEL:
SEE SECTION II, HAZARDOUS INGRIDIENTS
-KEPECTS OF OVEREXPOSURE: The Or Overkavisions:
INMALATION: itritation of the respiratory tract & acute narveus
system depression characterized by the following progressive
steps' headeche, disziness, staggering gait, confusion,
unconsciousness or

Appendix A-4b: Deft® Solvent-borne Epoxy Primer (Catalyst) MSDS Excerpt

Appendix A-5: Deft_® Solvent Epoxy Primer Product Information Data Sheet

PRODUCT INFORMATION DATA SHEET

BASE CHARACTERISTICS

CATALYST CHARACTERISTICS

i.

FREEZES

CHARACTERISTICS AS APPLIED INO REDUCTION

Wt./Gal.-------------------------- [10.35] VOC pounds per gallon-(2.82) VOC grams per liter-1 338)

Wt./Gal.of Solids------ (12.85 fbs) $sq./Ft.$ coverage Φ 1 Grams per sq./Ft. @ 1 mil dry---------------------------- (3.68 grams)

QUALIFIED TEST RESULTS

 $02 - Y - 40$ Page 2

EPOXY POLYAMIDE PRIMER DESCRIPTION AND APPLICATION INFORMATION **DESCRIPTION:**

Chemically cured two component epoxy-polyamide primer suitable for application on aircraft and acrospace equipment. Component, 1 contains the pigment and epoxy resin. Component 11 is the clear non-pigmented aliphatic polyamine-epoxy portion which acts as the hardener or curing agent for Component 1.

AIR POLLUTION REGULATIONS:

This product is formulated for use where the air pollution regulations call out for a maximum VOC of 340 grams per liter.

SPECIAL FEATURES:

This epoxy-polyamide primer is a solvent borne, corrosion inhibiting and chemical and solvent resistant primer

APPLICATION:

This primer will spray satisfactorily in all respects and shall show no running, sagging or streaking. The dry film shall show no dusting, mottling or color separation and shall present a smooth finish free from seeds. The standard film thickness shall be 0.6 to 0.9 mils dry.

Appendix B:

Deft_® 44-GN-72 Water-borne Epoxy Polyamide Primer (MIL-P-85582B)

 $=$ Flame AAS results

Appendix B-2: Water-borne Epoxy Particle Size Distributions by Flow Rate

Appendix B-3: Water-borne Epoxy Particle Sample DI [Cr⁶*] vs. Time

The chart above depicts the Cr^{6+} concentration data from the data summary table (Appendix B-1). Lines connect $[Cr]P$, the concentration of total $Cr⁶⁺$ collected (including that in particles) in each sample, to that sample's 1-hour ([Cr]NPl) and 24-hour ([Cr]NP24) concentration from dissociated Cr^{6+} (i.e. with particles removed).

Appendix B-4a: Deft® Water-borne Epoxy Primer (Base) MSDS Excerpt

MATERIAL SAFETY DATA SHEET Printed: 07/26/00 Page: 1 For Coatings, Resins and Related Materials --
Revised : 06/16/98 SECTION I - PRODUCT INDENTIFICATION Manufacturer: DEFT, DRC. (CAGE CODE 33461) Information Phone: (949) 474-0400
17451 VON KARMAN AVENUE (Phone: 1800) 424-9300
CHEMPIREC Phone: 800-424-9300 TOUTER: ra. 92614 Product Class: TYPE I.C. 2, EPOXY

Trade News : COMP.B BIL-F-85582 TYPE 1, CLA! 0 ---> extreme

Product Code : 44036072CAT

Product Code : 44036072CAT

Product Code : 44036072CAT

C.A.S. Namber: WOWN C.A.S. Munber: NOME SECTION II - HARARDOUS INGREDIENTS arasard a conservative por comme and making -------------- Exposure Limits --- $\begin{picture}(180,10) \put(0,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}} \put(15,0){\vector(1,0){100}}$ **COSHA STELL trus** $\overline{\mathbf{E}}$ **STEL** CAS $\#$ nm 193 Ingredients .
The contract of the contract of .
1991-1982 Water State, State Parks Ports, Maria Water izar suo statuso la N.B. 16 & 68F **MITROETHANE** $79 - 24 - 3$ 30. 100 ррн № №.Е. 100 ррж THE ABOVE LISTED PRODUCTS ARE ON THE TSCA INVENTORT LIST. MUSO ANY UNLISTED INCREDIENTS. N.R. - Not Established SECTION III - PHYSICAL DATA **Boiling Range: 237 - 300 Deg. P
Byap, Rate: 1.27 x n-Butyl Acetate
Volatiles vol 4 32.2 Wgt4 30.1** Vapor Density: Heavier than Air.
Liquid Bensity: Heavier than Mater. Wgt per gallon:
Spac. Gravity: 9.38 Founds. Appearance: MEER LIQUID NITH SOLVENT ODOR

V.O.C.: 345 G/L

SOLURILITY IN WATER: Insolute OR: With ANY MOTOR MOVING

MOVING TERRELATURE: No information found

MOVING TERRELATURE: No information found

DECOMPOSITY TERRELATU 1,12605 PH: Not spplicable COERGGION RATE: No information found
ViscosITT: Thin liquid to heavy viscous material SECTION IV - FIRE AND EXPLOSION HAZARD DATA Flammability Class: IC Flagh Point: 87 F TOC LEL; 3.40% UEL: 0.004 -EXTIMATIONING MEDIA: FORM, ALCOROL FORM, CO2, DRY CHEMICAL, WATER FOG-SPECIAL FIREFIGHTING FROCEDURES: -arminal rimerularing rmocentures:

Nail five fighting equiperent with self-contained breathing

sparatus and full protective clothing should be worn by fire

fighters. Water may be used to cool closed containers to preven NA PIEE & EXPLOSION HANANDS:
Leep containers tightly closed. Isolate from heat, sparks,
electrical equipment and open flame. Closed containers may
explode when exposed to extreme heat. Application to hot
surfaces requires .
In 1981 that the set through the sign and the through sign and the case in the second sign that the second the SECTION V - HEALTH HAZARD DATA -PERMISSINLE EXPOSURE LEVEL:
SEE SECTION II, HARARDOUS INGREDIENTS. -EFFECTS OF OVERECTORS:
THEMASTICH: ITTLEADS of the respiratory tract & acute nervous
system depression characterized by the following progressive
steps: beadache, dirimese, staggering gait, confusion, unconsciousness or comm. SKIN AND RYE CONDACT: SKIN: Contact with the skin can cause Sacritation. Symptoms may be swelling, redness, and rash.
EYES: Liquid, areosols, or vapors are irritating and may cause SKIN ABSORPTION: Prolonged or repeated contact can cause
moderate irritation, drying, and defatting of the skin which can cause the skin to crack. INGESTION: Acute: Can result in irritation and possible
corrosive action in the mouth, stomach tissue and digestive tract. Voniting may cause aspiration of the solvent, resulting
in chemical pneumonitis. HEALTH HAZARDS (ACUTE AND CHRONIC) numern numeros unces and canceroses, nose, and throat.
ACUTE: Vapors are irritating to eyes, nose, and throat.
Inhalation may cause beadaches, difficult breathing and loss of consciousness.

Appendix B-4b: Deft_® Water-borne Epoxy Primer (Catalyst) MSDS Excerpt

Appendix B-5: Deft® Water Epoxy Primer Product Information Data Sheet

PRODUCT INFORMATION DATA SHEET

MAR

BASE CHARACTERISTICS

VOC pounds/gallon--- (2.80) VOC grams per liter---- (333)

CHARACTERISTICS AS CATALYZED (NO REDUCTION) \mathbb{R}^2

 Wt/Gal of Solids--------- (12.06 lbs) Sq /Ft. coverage $@1$ Grams per sq./Ft.@1

% solids by weight-

% solids by volume
 (69.28%)
 $VOC pounds/gallon$ (2.87)

VOC grams per liter------------ 344 j

CATALYST CHARACTERISTICS

QUALIFIED TEST RESULTS

V.

Deft Product Information Data Sheet For 44-GN-072 (Proposed Color)

EPOXY POLYAMIDE, WATER REDUCIBLE PRIMER DESCRIPTION AND APPLICATION INFORMATION

DESSCRIPTION: Chemical cured two component epoxy polyamide water reducible primer for application on ferrous and non-ferrous metals. Component A contains the pigment and polyamide resin. Component B is the clear non-pigmented epoxy portion which acts as the hardener or curing agent for Component A.

AIR POLLUTION REGULATIONS: This product is formulated for use where the air pollution regulations call out for a maximum volatile organic compound (VOC) of 340 grams per liter.

SPECIAL FEATURES: This epoxy polyamide primer is a water reducible, corrosion inhibiting chemical and solvent resistant primer.

APPLICATION: This primer will spruy satisfactorily in all respects and shall show no running, sagging or streaking. The dry film shall show no dusting, monting or color separation and shall present a smooth finish free from seeds. The standard film thickness shall be 0.6 to 0.9 mils dry. MIXING INSTRUCTIONS

(Insurad: 3 / 997) -

 $\frac{\lambda_{\rm max}}{\lambda_{\rm max}}$

Appendix C:

Deft_® 09-Y-2 Elastomeric Polyurethane Primer (TT-P-2760A)

Appendix C-1: Polyurethane Data Summary

Appendix C-2: Polyurethane Particle Size Distributions by Flow Rate

Appendix C-3: Polyurethane Particle Sample DI [Cr⁶*] vs. Time

The chart above depicts the Cr^{6+} concentration data from the data summary table (Appendix C-1). Lines connect [Cr]P, the concentration of total Cr^{6+} collected (including that in particles) in each sample, to that sample's 1-hour ([Cr]NPl) and 24-hour ($[Cr]NP24$) concentration from dissociated $Cr⁶⁺$ (i.e. with particles removed).

Appendix C-4a: Deft_® Polyurethane Primer (Base) MSDS Excerpt

Page: 1 SECTION I - PRODUCT INDENTIFICATION Information Phone: (949) 474-6409
Emergency Phone: (800) 424-9300
CHEMPREC Phone: 800-424-9360 Namufacturer: DEFD, INC.X(CAGE CODE 33461)
17451 VON KARAAN AVENUE **TOUTMR** \mathbf{m} 92614 $\begin{array}{ll}\n & \text{Haarad Ratings:} & \text{Haacht} - 4 \\
 & \text{nons} \rightarrow \text{extrease} & \text{Fire} - 3 \\
 & 0 & \text{---} & 4 \\
 \end{array}$ Product Class: POLYURETHANE Personal Protection - I .
2010. Oli 2010. Oli 2010 por esperanto anno 1990 anno 1990 del 2010. Del 2010 del 2010 del 2010 del 2010 del - HAXARDOUS DATREDIENTS

CAS 1 Weight Theorem and the second of the second term of the second o SECTION II - HAZARDOUS INGREDIENTS $M^{\rm th}$ ma HG Ingredients 200 ppm 13 9 68F
N.B. .7 9 68F е повест вструмен ETHYL 3-ETHOLYPROPIONATE DISPERSION AID 150 ppm 5.1 0 689
125 ppm 7.1 0 68P **XYLENE** STHYL BENZENE N.E. 8.8 9 68F тялитит, массики. **ANYI-FLOAT AGENT**
STRONTION CHRONATE METHEL EVENTL KETOWE
2-4 PERTAMEDIONE 300ppm 70 # 68F
N.E. 6.9 # 68F DURFFÜLTIM DILABRATE $.2$ 4320 F THE ABOVE LISTED PRODUCTS ARE ON THE TSCA INVENTORY LIST. NE R. a Mot Retablished SECTION III - PHYSICAL DATA .
In 20th ESI (2011): 2011 124 135 136 137 138 139 239 230 130 131 132 133 134 135 137 138 139 130 130 130 130 Scaling Range: 175 - 401 Deg. F Waper Density: Heavier than Air.

Bog, Rate: 0.66 x n-Butyl Acetate Liquid Density: Heavier than Mater.

Vapearance: BROMM LIQUID WITH SOLVENT ODOR

9.0. Spec. Gravity: 1.38415

2010.0.: 262 **Scaling Range: 175 - 401 Deg. P**
Boap, Rate: 0.66 x n-Butyl Acetate
Volatiles vol % 28.4 Wgt% 19.0 CORROSION RATE: No information found
VISCOSITY: Thin liquid to heavy viscous material SECTION IV - FIRE AND EXPLOSION HAZARD DATA Plannability Class: IB
-EXTIMATISHING MEDIA: Flash Point:23 F TCC LEL: 1.00% UEL: 11.40% -EXTIMBUISHER MEDIA, FOR DRY CHEMICAL, WATER FOG
-SPECIAL PIRETORIAL PROCESSINGS:
-SPECIAL PIRETORITIES PROCESSINGS:
-SPECIAL PIRETORITIES PROCESSINGS:
-SPECIAL PIRETORITIES and full protective clothing should be worn by f UAL FIRE & EXPLOSION HAZARDS:

Resp containers tightly closed. Irolate from heat, sparks,

reprecised equipment and open flame. Closed containers may

explode when exposed to extreme heat. Application to hot

surfaces requ versions versions and .
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Appendix C-4b: Deft® Polyurethane Primer (Catalyst) MSDS Excerpt

PRODUCT INFORMATION DATA SHEET

BASE CHARACTERISTICS

CATALYST CHARACTERISTICS

CHARACTERISTICS AS APPLIED (NO REDUCTION)

QUALIFIED TEST RESULTS

- 1. Scope: (Para 1.1) This is a low Volatile Organic Compound (VOC), solvent borne, elastomeric, polyurethane primer coating. This primer coating is formulated primarily for spray application. It is compatible with polymethane topcoats and is intended for use on aircraft and other equipment subject to structural flexing at low temperatures.
- 2. Classification: (Para.1.2) The coating shall meet the following: Type I: Standard Pigments Class I: Strontium Chromate based corrosion inhibitors
-
- 3. Volatile Organic Compound (VOC) Centent: The maximum VOC content of this primer coating at application shall be 340 grams per liter (2.80 lbs. per gallon). The resistivity of the solvents shall be suitable for electrostatic application.
- 4. Condition In Container: (3.5.1) The coating components shall be capable of being easily mixed by hand, with a paddle, to a smooth, homogeneous, pourable condition and free from gelation.
- 5. Storage Stability: (Para 3.5.2) The previously unopened packaged material shall be capable of meeting all requirements specified for a period of one year, when stored in an area where the daily temperature of the ambient air is with-in the range of (1.7°C to 46°C (35°F to 115°F).

Page 1 of 4

 $(1$ mund: $6/97$

POLYURETHANE DESCRIPTION AND APPLICATION INFORMATION

DESCRIPTION: Chemically cured two component polyurethane elastomeric primer suitable for application on aircraft and aerospace equipment. Component A. contains the pigment and the oil-free polyester resin. Component B is the clear non-pigmented aliphatic isocyanate prepolymer portion which acts as the hardener or curing agent for Component A.

PIGMENTS: Shall have exterior durability and be lead free.

AIR POLLUTION REGULATIONS: This product is suitable for use where the air pollution regulations call out for a maximum VOC of 340 grams per liter or les

SURFACE PREPARATION: This product is designed for use over deoxidized aluminum, chromic acid anodized aluminum, sulfuric acid anodized aluminum, titanium, magnesium, steel, fiberglass, and Alodine 1000, 1200 and 1500 equivalent pre treatments.

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Appendix D: Particle Distribution Smoothing

The assumptions that all particles collected in the $\geq 20 \,\mu m$ bin (i.e. all particles collected in the range $\geq 20 \mu m < 125 \mu m$) had a particle diameter of 20 μ m or that the bin had a midpoint of $(125 \mu m - 20 \mu m)/2$ were deemed inaccurate. As a result, extrapolation of particles counted in the 20 μ m bin was chosen as the method to smooth the solvent- and water-borne epoxy particle size distributions. This was accomplished using "virtual" bins in $1.5 \mu m$ bin size increments (the same increment used in the actual particle counts). Extrapolations are based on the percentage change of particle numbers in the last three bins prior to the $\geq 20 \mu m$ bin. More specifically, the trend in the difference (Δ) between successive bin particle number concentrations $(N_i's)$, beginning with the 15.5 μ m (N₁₂) bin, was used to weight the decrease for each succeeding bin as in equation A-1. N_i's were computed starting with the 20 μ m bin (N₁₅), and extrapolation ceased once the number of particles in the pre-extrapolation $20 \mu m$ bin was exhausted.

$$
N_{i} = N_{i-1} - \left(\frac{(N_{i-3} - N_{i-2}) - (N_{i-2} - N_{i-1})}{N_{i-3} - N_{i-2}}\right) \cdot (N_{i-2} - N_{i-1})
$$
(A-1)

where: $i =$ the discrete bin number such that $i - 1$ is the previous bin and i - 2 the bin before that, etc.

For example, given a set of collected particle counts and the differences (ΔN_i) beginning with bin 12 (as shown in the table below):

The first extrapolation is performed for bin 15 as follows:

$$
N_{15} = N_{14} - \left(\frac{(N_{12} - N_{13}) - (N_{13} - N_{14})}{N_{12} - N_{13}}\right) \cdot (N_{13} - N_{14}) = 110 - \left(\frac{(50) - (40)}{(50)}\right) \cdot (40) = 78
$$

This is continued for bins 16 and higher until the 300 particles/mL counted in the original bin 15 (\geq 20 μ m) are exhausted, so that the resulting table looks like:

Note: counts/mL are rounded

Many of the polyurethane samples showed either an upward or incoherent trend in $bins > 11 \mu m$. For these distributions, extrapolations assumed the 20 μ m bin to have the same N as the $18.5 \mu m$ bin and then a linear decrease was applied to determine the remaining N_i 's.

Appendix E: Aerodynamic Diameter and Cr⁶* Volume Calculations

Converting bin midpoint d_p , (denoted as the bold d_p), to an equivalent d_{ae} , and

determining the Cr⁶⁺ % volume for each particle size first required computation of ρ_p ,

(denoted as the bold p_p) the density specific to each d_p . The steps used in the

calculations are shown below (1-3 correspond with the conceptual diagram in Chapter 4).

Examples calculations are shown for the solvent-borne epoxy $8 \mu m$ particle size bin

(midpoint $8.75 \,\mathrm{\upmu m}$).

Step₁

Using Table 16, linearly interpolate the mass fraction of Cr (mean % Cr) in a *dry* paint particle for the bin midpoint size, d_p , using effective cutoff diameter (ECD) as an estimate of d_p .

$$
m_{Cr,d_p} = \left(\frac{d_p - ECD_1}{ECD_2 - ECD_1}\right) \cdot (%Cr_2 - %Cr_1) + %Cr_1
$$
 (E-1)

where: $m_{Cr,dp}$ = (mass of Cr)/(mass of *dry* paint) in a particle of size d_p [Table 16] d_p = particle size bin midpoint diameter ECD_1 = closest ECD (from Table 16) to $\mathbf{d}_{\mathbf{p}}$ that is smaller than $\mathbf{d}_{\mathbf{p}}$ ECD₂ = closest ECD (from Table 16) to $\mathbf{d}_{\mathbf{p}}$ that is larger than $\mathbf{d}_{\mathbf{p}}$ $\%Cr_1$ = (mass of Cr)/(mass of *dry* paint) corresponding to ECD₁ [Table 16] $\%Cr_2$ = (mass of Cr)/(mass of *dry* paint) corresponding to ECD₂ [Table 16]

$$
m_{Cr,8.75\mu\text{m}} = \left(\frac{8.75\mu\text{m} - 7.0\mu\text{m}}{9.5\mu\text{m} - 7.0\mu\text{m}}\right) \cdot (5.3\% - 4.6\%) + 4.6\% = 5.09\% \approx .0509
$$

Step 2a

Convert the mass fraction of Cr in a $\frac{dy}{dt}$ paint particle of size \mathbf{d}_{p} , interpolated from Table 16, to the mass fraction of Cr in a *wet* droplet (particle) of size d_p .

$$
\mathbf{M}_{\mathrm{Cr},\mathbf{d}_{\mathrm{p}}} = \mathbf{m}_{\mathrm{Cr},\mathbf{d}_{\mathrm{p}}} \cdot \mathbf{v}_{\mathrm{solids}} \cdot \left(\frac{?_{\mathrm{dry}}}{?_{\mathrm{wet}}}\right) \tag{E-2a}
$$

where: $M_{Cr\,d_p}$ m_{Cr,\mathbf{d}_P} Vsolids Pdry Pwet $=$ (mass of Cr)/(mass of *wet* paint) in a particle of size d_p $=$ (mass of Cr)/(mass of *dry* paint) in a particle of size d_p [Table 16] $=$ (Vol. of dry paint)/(Vol. of wet paint) [Table 15] = density of dry paint \approx solids density (g/L) [Table 15] = density of the total wet paint mixture (g/L) [Table 15]

Example 2a

$$
M_{Cr,8.75\mu m} = 0.0509 \frac{g Cr}{g dry paint} \cdot .5855 \frac{L \text{ solids}}{L \text{ paint}} \cdot \left(\frac{1539.8 \frac{g}{L dry paint}}{1240.2 \frac{g}{L wet paint}}\right) = 0.0370 \frac{g Cr}{g wet paint}
$$

Step 2b

Convert the mass fraction of Cr in a *wet* particle of size d_p to a mass fraction of SrCrO₄ in a *wet* particle of size d_p.

$$
m_{srcro_4, d_p} = M_{cr, d_p} \cdot \left(\frac{MW_{srcro_4}}{MW_{cr}}\right)
$$
 (E-2b)

where: $m_{SrCrO4, dP} = (mass of SrCrO₄)/(mass of wet paint)$ in a particle of size d_p MW_{SrCrO4} = molecular weight of SrCrO₄ (204 g/mol) MW_{Cr} = molecular weight of Cr (52 g/mol)

Example 2b

$$
m_{\text{SrCo4,875}\mu\text{m}} = 0.0370 \frac{\text{g Cr}}{\text{g wet paint}} \cdot \left(\frac{204 \text{ g/mol}}{52 \text{ g/mol}}\right) = 0.1452 \frac{\text{g SrCrO}_4}{\text{g wet paint}}
$$

Step 3

Convert the mass fraction of $SrCrO₄$ in a *wet* particle of size d_p to a *volume* fraction of $SrCrO₄$ in a *wet* particle of size d_p .

$$
v_{srcro_4, d_p} = m_{srcro_4, d_p} \cdot \left(\frac{?_{wet}}{?_{srcro_4}}\right)
$$
 (E-3)

where: $V_{SrCrO4,dp}$ ρ_{SrCrO4} $=$ (Vol. of SrCrO₄)/(Vol. of wet paint) in a particle of size d_p $=$ density of SrCrO₄ (3900 g/L)

Example 3

$$
v_{SrCrO_4,8.75\mu m} = 0.1452 \frac{g SrCrO_4}{g wet paint} \cdot \left(\frac{1240.2 \frac{g}{L wet paint}}{3900 \frac{g}{L SrCrO_4}}\right) = 0.04616 \frac{L SrCrO_4}{L wet paint}
$$

Step 4

Calculate ρ_p , the density of a wet paint particle of size d_p .

$$
\mathbf{?}_{\mathbf{p}} = [\mathbf{v}_{\text{SrCO}_4,\mathbf{d}_{\mathbf{p}}}] \cdot \mathbf{?}_{\text{SrCO}_4} + [1 - \mathbf{v}_{\text{SrCO}_4,\mathbf{d}_{\mathbf{p}}}] \cdot \mathbf{?}_{\text{non-SrCO}_4}
$$
(E-4)

where: $\rho_{\text{non-SrCro4}}$ = the combined density of all the non-SrCrO₄ paint constituents in the paint mixture, such that: $\rho_{\text{non-SrCrO4}} = \rho_{\text{wet}} - (\rho_{\text{SrCrO4}} \mathbb{I} \text{ vol. fraction of SrCrO}_4 \text{ in the total},$

homogenous, paint mixture)

$$
?8.75 \,\mathrm{\mu m} = \left[0.04616 \frac{\text{L SrCrO}_4}{\text{L wet paint}} \right] \cdot 3900 \frac{\text{g}}{\text{L SrCrO}_4} + \left[1 - 0.04616 \frac{\text{L SrCrO}_4}{\text{L wet paint}} \right] \cdot 988.3 \frac{\text{g}}{\text{L non-SrCrO}_4}
$$

$$
= 1123 \frac{\text{g}}{\text{L}}
$$

Step 5

Calculate a terminal settling velocity (v_t) for the wet droplet of size d_p by applying ρ_p to the Stokes equation.

$$
v_t = \frac{C_c^2 \rho d_p^2}{18 \cdot \mu} \cdot g \tag{E-5}
$$

where: C_c = Cunningham Slip Correction factor (unitless) [diameterdependent]; values ranged from 1.326 to 1.008 for collected particle sizes μ = dynamic viscosity of air (g/cm·s) [temperature-dependent] g_{\parallel}

= acceleration due to gravity cm/s^2)

Example 5

$$
v_{\tau} = \frac{(1.02) \cdot \left(1123 \frac{g}{L}\right) \cdot (8.75 \,\mu\text{m})^2 \cdot \left(\frac{L}{1000 \,\text{cm}^3}\right) \cdot \left(\frac{\text{cm}^2}{1 \cdot 10^8 \,\mu\text{m}^2}\right)}{18 \cdot \left(1.85 \cdot 10^{-4} \frac{g}{\text{cm} \cdot \text{s}}\right)}
$$
 (980 $\frac{\text{cm}}{\text{s}^2}$)

$$
= .2581 \frac{\text{cm}}{\text{s}} = 2581 \frac{\text{\mu m}}{\text{s}}
$$

Step 6

Calculate d_{ae} by solving for diameter given the computed v_t and $p_p = 1$ g/cm³ (unit density).

$$
d_{ae} = \sqrt{\frac{v_t \cdot (18 \cdot \mu)}{C_c \cdot ?_p \cdot g}}
$$
(E-6)

$$
d_{ae} = \sqrt{\frac{\left(2581 \frac{\mu m}{s}\right) \cdot 18 \cdot \left(1.85 \cdot 10^{-4} \frac{g}{cm \cdot s}\right) \cdot \left(\frac{cm}{1 \cdot 10^{4} \mu m}\right)}{(1.02) \cdot \left(1 \frac{g}{cm^{3}}\right) \cdot \left(980 \frac{cm}{s^{2}}\right) \cdot \left(\frac{cm^{3}}{1 \cdot 10^{12} \mu m^{3}}\right) \cdot \left(\frac{1 \cdot 10^{4} \mu m}{cm}\right)} = 9.3 \mu m
$$

Step 7
Coloulate the volume fraction of C^{6+} Calculate the volume fraction of Cr^{6+} (as a % volume) in a wet particle of size d_p by applying ρ_p .

$$
v_{Cr, d_p} = m_{SrCrO_4, d_p} \cdot \left(\frac{MW_{Cr}}{MW_{SrCrO_4}}\right) \cdot \left(\frac{?_{p}}{?_{Cr}}\right) \times 100\%
$$
 (E-7)

where: v_{Cr, d_P} = (Vol. of Cr)/(Vol. of wet paint) in a particle of size d_p (as a % vol.) ρ_{Cr} = density of Cr (7190 g/L)

$$
v_{Cr,8.75\mu m} = 0.1452 \frac{g \text{ SrCrO}_4}{g \text{ wet paint}} \cdot \left(\frac{52 \text{ g/mol}}{204 \text{ g/mol}}\right) \cdot \left(\frac{1123 \frac{g}{L}}{7190 \frac{g}{L}}\right) \times 100\% = 0.58\% \leftarrow \frac{\text{Cr Volume}}{\text{Particle Volume}}
$$

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Vita

Captain Richard A. Schilke was born in Elyria, Ohio and graduated from Elyria Catholic High School in June 1988. On 26 May 1993 he graduated from the U. S. Naval Academy, receiving a Bachelor of Science degree in Oceanography and a commission as a 2nd Lt. in the U. S. Marine Corps (USMC). After training at The Basic School, Marine Corps Base (MCB) Quantico, Virgina, he reported to Naval Air Station Pensacola, Florida for Naval Flight Officer training. In April 1996, 1st Lt. Schilke received his wings of gold and proceeded to Marine Corps Air Station (MCAS) El Toro, California to train in the F/A-18D Hornet as a Weapons and Sensors Officer (WSO). In April 1997, he reported to Marine All-Weather Fighter Attack Squadron 332 [VMFA(AW)-332], MCAS Beaufort, South Carolina. There he served as the Naval Aviation Training and Operating Procedures Standardization Officer and was promoted to Captain in July 1997. In July 1998, Captain Schilke joined VMFA(AW)-533. From August 1998 to March 1999 he deployed to the Western Pacific with VMFA(AW)-533 and served as the squadron Maintenance Training Division Officer. There he participated in joint and combined exercises, and earned qualification as a squadron Air Combat Tactics Instructor. In May 1999, his squadron deployed to Taszar Air Base, Hungary as part of Combined Joint Task Force Noble Anvil. There he flew combat missions into Serbia and Kosovo in support of Operation Allied Force. Captain Schilke remained in VMFA(AW)-533 until August 2000, serving as the Current and Future Operations Officer and graduating from the U. S. Navy Fighter Weapons School (TopGun). In August 2000, he entered the Graduate School of Engineering and Management, Air Force Institute of Technology and upon graduation will be assigned as the Deputy, Natural Resources and Environmental Affairs Branch, Facilities Division, MCB Quantico, Virginia. Captain Schilke's personal awards include the Strike Flight Air Medal and the Navy and Marine Corps Commendation Medal with Combat V.

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